

Predicting Fick- and Maxwell-Stefan diffusivities in liquids

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Fluid Phase Equilibria, 2011, 301, 110-117.

Chem. Phys. Lett., 2011, 504, 199-201.

J. Phys. Chem B, 2011, 115, 8506-8517.

J. Phys. Chem B, 2011, 115, 10911-10918.

J. Phys. Chem B, 2011, 115, 12921-12929.

Ind. Eng. Chem. Res., 2011, 50, 4776-4782.

Ind. Eng. Chem. Res., 2011, 50, 10350-10358.

Collaborators

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(Empirical) Fick formulation for multicomponent diffusion

$$J_i = -c_t \sum_{k=1}^{n-1} D_{ik} \nabla x_k$$

- n components, $(n - 1)^2$ Fick diffusivities
- $\sum_{i=1}^n J_i = 0$ (molar reference frame)
- $D_{ij} \neq D_{ji}$ for $n > 2$
- D_{ij} strongly dependent on the mole fractions $x_1 \cdots x_n$
- D_{ij} can become negative for $n > 2$
- multicomponent D_{ij} unrelated to binary counterpart
- R. Krishna and J.A. Wesselingh, Chem. Eng. Sci., 1997, 52, 861-911.

Maxwell-Stefan formulation at constant T, p

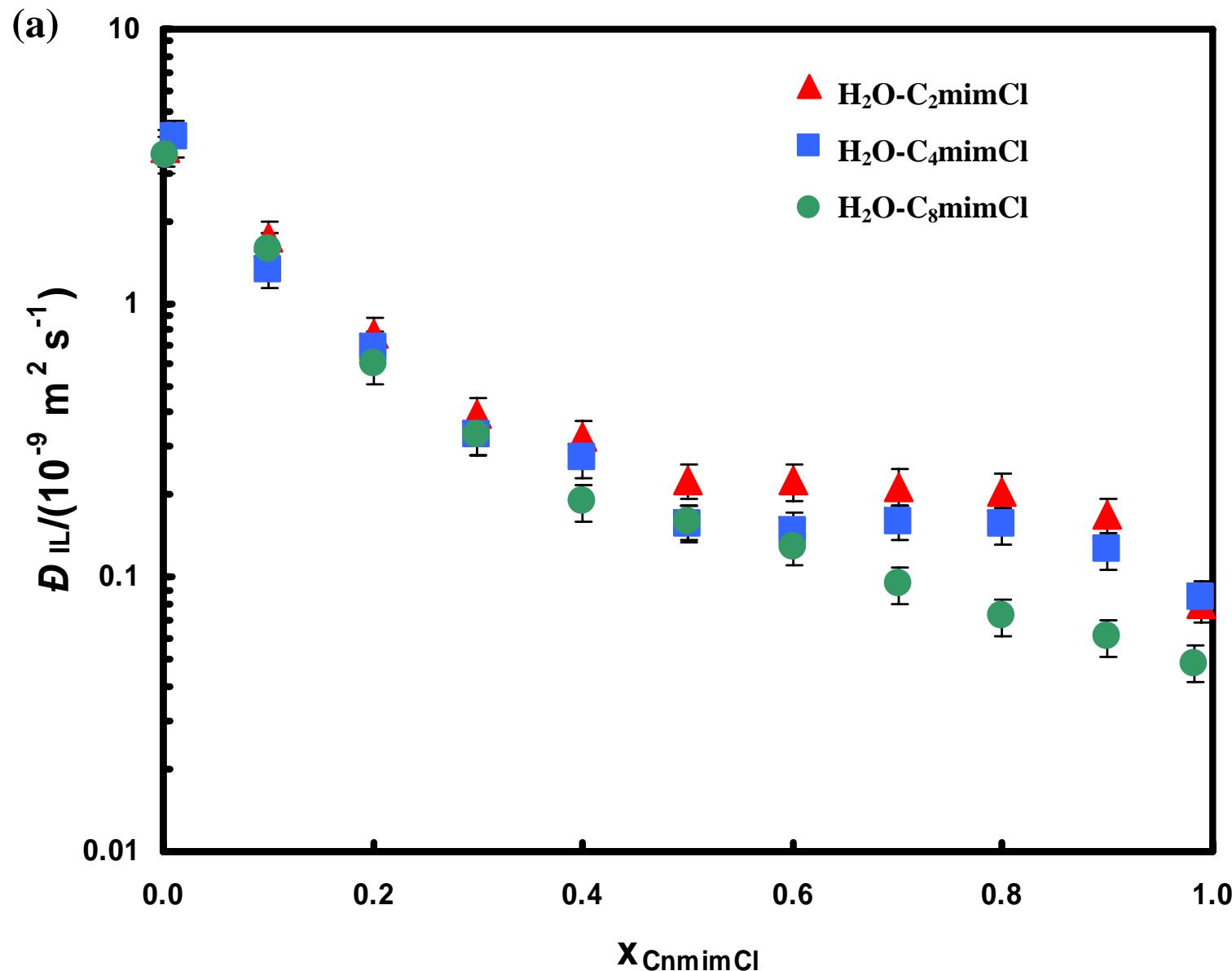
$$d_i = \frac{x_i \nabla \mu_i}{RT} = \sum_{j=1, j \neq i}^n \frac{x_i x_j (u_j - u_i)}{\mathcal{D}_{ij}} = \sum_{j=1, j \neq i}^n \frac{x_i J_j - x_j J_i}{c_t \mathcal{D}_{ij}}$$

$$J_i = u_i c_i = u_i x_i c_t$$

$$\sum_{i=1}^n x_i \nabla \mu_i = 0$$

- Gradient in chemical potential as driving force d_i
- n components, $n(n - 1)/2$ MS diffusivities, $\mathcal{D}_{ij} > 0$
- $\mathcal{D}_{ij} = \mathcal{D}_{ji}$ (Onsager's reciprocal relations)
- \mathcal{D}_{ij} is less composition dependent than Fick diffusivities
- Possibility to predict \mathcal{D}_{ij} using theory...

Diffusion coefficients depend on concentration!



Vignes equation in ternary systems

$$\mathcal{D}_{ij} \approx (\mathcal{D}_{ij}^{x_i \rightarrow 1})^{x_i} (\mathcal{D}_{ij}^{x_j \rightarrow 1})^{x_j} (\mathcal{D}_{ij}^{x_k \rightarrow 1})^{x_k}$$

- Recommended in chemical engineering
- Is it any good?
- What about $\mathcal{D}_{ij}^{x_k \rightarrow 1}$? Models for this in literature:

WK (1990) $\mathcal{D}_{ij}^{x_k \rightarrow 1} = \sqrt{\mathcal{D}_{ij}^{x_j \rightarrow 1} \mathcal{D}_{ij}^{x_i \rightarrow 1}}$

KT (1991) $\mathcal{D}_{ij}^{x_k \rightarrow 1} = \sqrt{\mathcal{D}_{ik}^{x_k \rightarrow 1} \mathcal{D}_{jk}^{x_k \rightarrow 1}}$

VKB (2005) $\mathcal{D}_{ij}^{x_k \rightarrow 1} = \left(\mathcal{D}_{ik}^{x_k \rightarrow 1} \right)^{\frac{x_i}{x_i+x_j}} \left(\mathcal{D}_{jk}^{x_k \rightarrow 1} \right)^{\frac{x_j}{x_i+x_j}}$

DKB (2005) $\mathcal{D}_{ij}^{x_k \rightarrow 1} = \frac{x_j}{x_i + x_j} \mathcal{D}_{ik}^{x_k \rightarrow 1} + \frac{x_i}{x_i + x_j} \mathcal{D}_{jk}^{x_k \rightarrow 1}$

RS (2007) $\mathcal{D}_{ij}^{x_k \rightarrow 1} = (\mathcal{D}_{ik}^{x_k \rightarrow 1} \mathcal{D}_{jk}^{x_k \rightarrow 1} \mathcal{D}_{ij}^{x_j \rightarrow 1} \mathcal{D}_{ij}^{x_i \rightarrow 1})^{1/4}$

(Open?) Questions

- Is the quality of Vignes increased/decreased by a particular model choice for $D_{ij}^{x_k \rightarrow 1}$?
- Which of the predictive models for $D_{ij}^{x_k \rightarrow 1}$ is best for a certain system? (if any...)
- VKB and DKB suggest that $D_{ij}^{x_k \rightarrow 1}$ does not exist, *i.e.* its value depends on the ratio x_i/x_j . Is this correct?

$$\text{WK (1990)} \quad D_{ij}^{x_k \rightarrow 1} = \sqrt{D_{ij}^{x_j \rightarrow 1} D_{ij}^{x_i \rightarrow 1}}$$

$$\text{KT (1991)} \quad D_{ij}^{x_k \rightarrow 1} = \sqrt{D_{ik}^{x_k \rightarrow 1} D_{jk}^{x_k \rightarrow 1}}$$

$$\text{VKB (2005)} \quad D_{ij}^{x_k \rightarrow 1} = \left(D_{ik}^{x_k \rightarrow 1} \right)^{\frac{x_i}{x_i+x_j}} \left(D_{jk}^{x_k \rightarrow 1} \right)^{\frac{x_j}{x_i+x_j}}$$

$$\text{DKB (2005)} \quad D_{ij}^{x_k \rightarrow 1} = \frac{x_j}{x_i + x_j} D_{ik}^{x_k \rightarrow 1} + \frac{x_i}{x_i + x_j} D_{jk}^{x_k \rightarrow 1}$$

$$\text{RS (2007)} \quad D_{ij}^{x_k \rightarrow 1} = (D_{ik}^{x_k \rightarrow 1} D_{jk}^{x_k \rightarrow 1} D_{ij}^{x_j \rightarrow 1} D_{ij}^{x_i \rightarrow 1})^{1/4}$$

Obtaining Maxwell-Stefan diffusivities from MD

$$\begin{aligned}
 \Lambda_{ij} &= \frac{1}{6N} \lim_{m \rightarrow \infty} \frac{1}{m \cdot \Delta t} \left\langle \left(\sum_{l=1}^{N_i} (r_{l,i}(t + m \cdot \Delta t) - r_{l,i}(t)) \right) \times \right. \\
 &\quad \left. \left(\sum_{k=1}^{N_j} (r_{k,j}(t + m \cdot \Delta t) - r_{k,j}(t)) \right) \right\rangle \\
 &= \frac{1}{3N} \int_0^\infty dt \left\langle \sum_{l=1}^{N_i} v_{l,i}(0) \cdot \sum_{k=1}^{N_j} v_{k,j}(t) \right\rangle
 \end{aligned}$$

Note: $\Lambda_{ij} = \Lambda_{ji}$ (Onsager)

Krishna & Van Baten, Ind. Eng. Chem. Res., 2005, 44, 6939-6947.

Obtaining ternary Maxwell-Stefan diffusivities from MD

$$\begin{aligned}
 D_{12} &= \frac{A + (x_1 + x_3) \frac{B}{C}}{x_1 D} \\
 A &= -\Lambda_{11}\Lambda_{23}x_2 - \Lambda_{12}x_3\Lambda_{21} + \Lambda_{11}x_3\Lambda_{22} - \Lambda_{11}x_3x_2\Lambda_{22} + \Lambda_{11}\Lambda_{23}x_2^2 - \Lambda_{11}x_3x_2\Lambda_{32} \\
 &\quad + \Lambda_{11}\Lambda_{33}x_2^2 - \Lambda_{13}x_1\Lambda_{22} - x_1x_3\Lambda_{11}\Lambda_{22} + \Lambda_{13}\Lambda_{22}x_1^2 - x_1\Lambda_{31}x_3\Lambda_{22} + \Lambda_{33}x_1^2\Lambda_{22} \\
 &\quad + \Lambda_{12}\Lambda_{23}x_1 + \Lambda_{12}x_3x_2\Lambda_{21} + \Lambda_{13}x_1x_2\Lambda_{22} + \Lambda_{12}x_3\Lambda_{31}x_2 + \Lambda_{13}x_2\Lambda_{21} - \Lambda_{13}x_2^2\Lambda_{21} \\
 &\quad - \Lambda_{13}x_2^2\Lambda_{31} + x_1\Lambda_{12}x_3\Lambda_{21} - x_1^2\Lambda_{12}\Lambda_{23} + x_1\Lambda_{32}x_3\Lambda_{21} - x_1^2\Lambda_{32}\Lambda_{23} + \Lambda_{13}x_1x_2\Lambda_{32} \\
 &\quad + x_1\Lambda_{11}\Lambda_{23}x_2 + x_1\Lambda_{31}\Lambda_{23}x_2 - \Lambda_{12}x_1\Lambda_{23}x_2 - \Lambda_{12}x_1\Lambda_{33}x_2 - x_1\Lambda_{13}x_2\Lambda_{21} \\
 &\quad - x_1\Lambda_{33}x_2\Lambda_{21} \\
 B &= \Lambda_{12}x_3 - \Lambda_{13}x_2 - x_1x_3\Lambda_{12} + x_1x_2\Lambda_{23} - x_1x_3\Lambda_{32} + x_1x_2\Lambda_{33} \\
 C &= -\Lambda_{11}\Lambda_{23}x_2 - \Lambda_{12}\Lambda_{21}x_3 + x_3\Lambda_{11}\Lambda_{22} - x_2x_3\Lambda_{11}\Lambda_{22} + \Lambda_{11}\Lambda_{23}x_2^2 - x_2x_3\Lambda_{11}\Lambda_{32} \\
 &\quad + \Lambda_{11}\Lambda_{33}x_2^2 - \Lambda_{13}\Lambda_{22}x_1 - x_1x_3\Lambda_{11}\Lambda_{22} + x_1^2\Lambda_{13}\Lambda_{22} - x_1x_3\Lambda_{31}\Lambda_{22} + x_1^2\Lambda_{22}\Lambda_{33} \\
 &\quad + x_1\Lambda_{12}\Lambda_{23} + x_2x_3\Lambda_{12}\Lambda_{21} + x_1x_2\Lambda_{13}\Lambda_{22} + x_2x_3\Lambda_{12}\Lambda_{31} + x_2\Lambda_{13}\Lambda_{21} - x_2^2\Lambda_{13}\Lambda_{21} \\
 &\quad - x_2^2\Lambda_{13}\Lambda_{31} + x_1x_3\Lambda_{12}\Lambda_{21} - x_1^2\Lambda_{12}\Lambda_{23} + x_1x_3\Lambda_{32}\Lambda_{21} - x_1^2\Lambda_{32}\Lambda_{23} + x_1x_2\Lambda_{13}\Lambda_{32} \\
 &\quad + x_1x_2\Lambda_{11}\Lambda_{23} + x_1x_2\Lambda_{31}\Lambda_{23} - x_1x_2\Lambda_{12}\Lambda_{23} - x_1x_2\Lambda_{12}\Lambda_{33} - x_1x_2\Lambda_{13}\Lambda_{21} \\
 &\quad - x_1x_2\Lambda_{33}\Lambda_{21} \\
 D &= \Lambda_{22}x_3 - \Lambda_{23}x_2 - \Lambda_{22}x_3x_2 + \Lambda_{23}x_2^3 - x_2\Lambda_{12}x_3 + \Lambda_{13}x_2^2 - x_2\Lambda_{32}x_3 + \Lambda_{33}x_2^2
 \end{aligned}$$

Limit when $x_k \rightarrow 1$ (1)

$$\begin{aligned}
\Lambda_{ii} &= \frac{1}{3N} \int_0^\infty dt \left\langle \sum_{l=1}^{N_i} v_{l,i}(0) \cdot \sum_{g=1}^{N_i} v_{g,i}(t) \right\rangle \\
&\approx \frac{N_i}{3N} \int_0^\infty dt \langle v_{i,1}(0) \cdot v_{i,1}(t) \rangle \\
&= x_i C_{ii} \\
\Lambda_{kk} &= \frac{1}{3N} \int_0^\infty dt \left\langle \sum_{l=1}^{N_k} v_{l,k}(0) \cdot \sum_{g=1}^{N_k} v_{g,k}(t) \right\rangle \\
&= \frac{1}{3N} \int_0^\infty dt \left\langle \sum_{l=1}^{N_k} v_{l,k}(0) \cdot v_{l,k}(t) \right\rangle + \frac{1}{3N} \int_0^\infty dt \left\langle \sum_{l=1}^{N_k} \sum_{g=1, g \neq l}^{N_k} v_{l,k}(0) \cdot v_{g,k}(t) \right\rangle \\
&\approx x_k C_{kk} + x_k^2 N C_{kk}^* \\
\Lambda_{ij, j \neq i} &= \frac{1}{3N} \int_0^\infty dt \left\langle \sum_{l=1}^{N_i} v_{l,i}(0) \cdot \sum_{k=1}^{N_j} v_{k,j}(t) \right\rangle \\
&\approx \frac{N_i N_j}{3N} \int_0^\infty dt \langle v_{1,i}(0) \cdot v_{1,j}(t) \rangle \\
&= N x_i x_j C_{ij}
\end{aligned}$$

Limit when $x_k \rightarrow 1$ (2)

Set $a = x_j/x_i$ and $x_k = 1 - x_i - x_j$, fill in the equations for Λ_{ii} , Λ_{jj} , Λ_{kk} , Λ_{ij} , Λ_{ik} , Λ_{jk} and take the limit $x_k \rightarrow 1$

Final result (after a lot of math):

Limit when $x_k \rightarrow 1$ (2)

Set $a = x_j/x_i$ and $x_k = 1 - x_i - x_j$, fill in the equations for Λ_{ii} , Λ_{jj} , Λ_{kk} , Λ_{ij} , Λ_{ik} , Λ_{jk} and take the limit $x_k \rightarrow 1$

Final result (after a lot of math):

$$\begin{aligned} D_{ij}^{x_k \rightarrow 1} &= \frac{D_{i,\text{self}}^{x_k \rightarrow 1} \cdot D_{j,\text{self}}^{x_k \rightarrow 1}}{D_{k,\text{self}}^{x_k \rightarrow 1} + C_x} \\ C_x &= N(C_{ij} - C_{ik} - C_{jk} + C_{kk}^*) \end{aligned}$$

which is independent of x_j/x_i !! (Note: C_x converges to a finite value when $N \rightarrow \infty$).

When cross-correlation are neglected:

$$D_{ij}^{x_k \rightarrow 1} \approx \frac{D_{i,\text{self}}^{x_k \rightarrow 1} \cdot D_{j,\text{self}}^{x_k \rightarrow 1}}{D_{k,\text{self}}^{x_k \rightarrow 1}}$$

Ternary system of WCA particles that only differ in mass

	MS diffusivity $\mathcal{D}_{12}^{x_3 \rightarrow 1}$						
	incl. C_x	$C_x = 0$	WK	KT	VKB	DKB	RS
Prediction	1.401	1.441	1.296	0.952	0.952	0.952	1.111
MD ^b	1.411	1.411	1.411	1.411	1.411	1.411	1.411
AD ^a	1%	2%	8%	32%	32%	32%	21%
Prediction	0.310	0.315	0.390	0.248	0.248	0.248	0.311
MD ^c	0.318	0.318	0.318	0.318	0.318	0.318	0.318
AD ^a	2%	1%	23%	22%	22%	22%	2%
Prediction	3.344	3.288	1.296	0.682	0.682	0.683	0.940
MD ^d	3.348	3.348	3.348	3.348	3.348	3.348	3.348
AD ^a	0%	2%	61%	80%	80%	80%	72%
Prediction	0.172	0.161	0.389	0.101	0.101	0.101	0.198
MD ^e	0.172	0.172	0.172	0.172	0.172	0.172	0.172
AD ^a	0%	7%	126%	42%	42%	42%	15%

^a absolute difference normalized with corresponding value from MD simulations

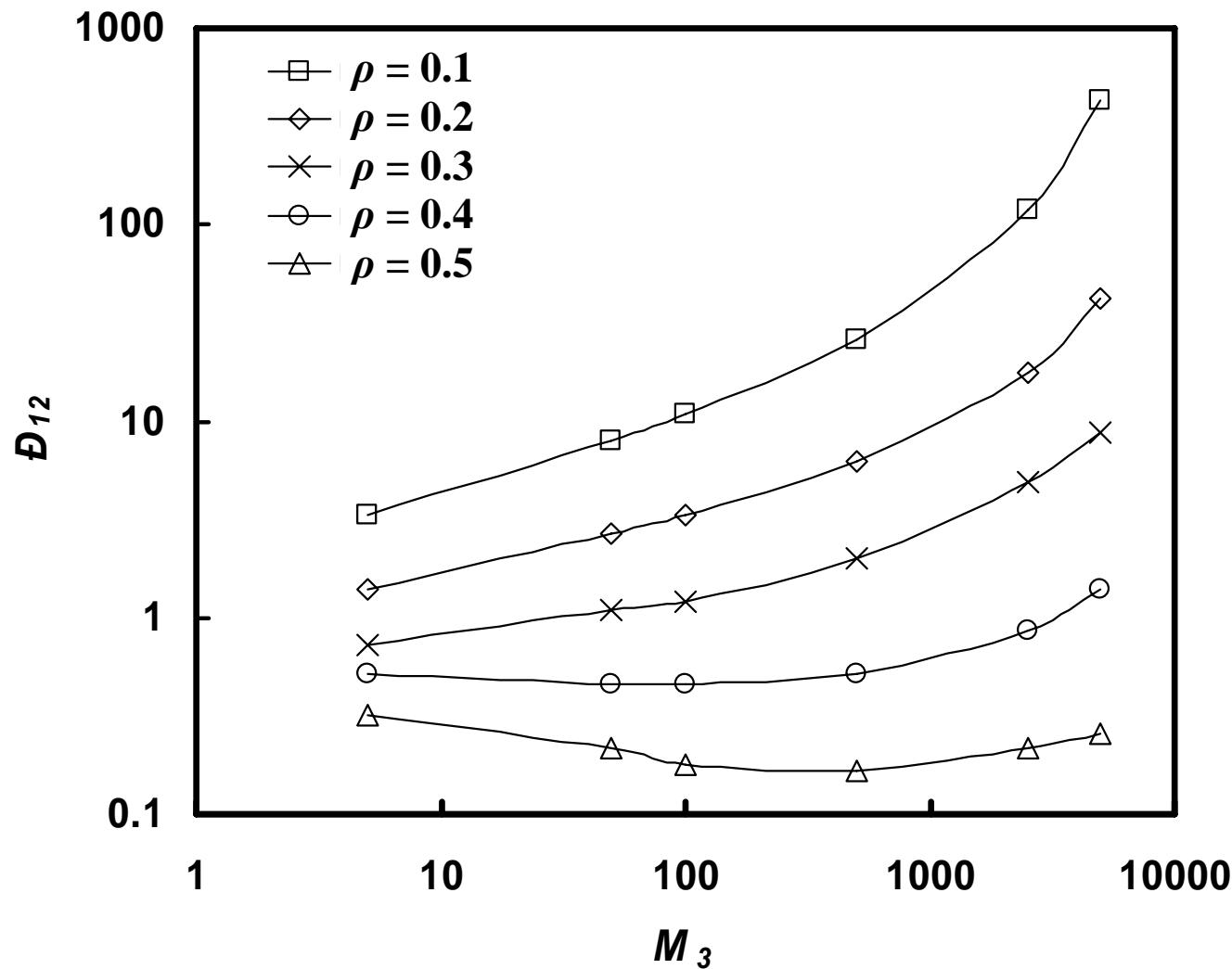
^b $\rho = 0.2$; $M_1 = 1$; $M_2 = 1.5$; $M_3 = 5$; $x_1/x_2 = 1$; $x_3 = 0.95$; $T = 2$

^c $\rho = 0.5$; $M_1 = 1$; $M_2 = 1.5$; $M_3 = 5$; $x_1/x_2 = 1$; $x_3 = 0.95$; $T = 2$

^d $\rho = 0.2$; $M_1 = 1$; $M_2 = 1.5$; $M_3 = 100$; $x_1/x_2 = 1$; $x_3 = 0.95$; $T = 2$

^e $\rho = 0.5$; $M_1 = 1$; $M_2 = 1.5$; $M_3 = 100$; $x_1/x_2 = 1$; $x_3 = 0.95$; $T = 2$

Increasing the mass of the solvent (M_3)



$$D_{ij}^{x_k \rightarrow 1} \approx \frac{D_{i,\text{self}}^{x_k \rightarrow 1} \cdot D_{j,\text{self}}^{x_k \rightarrow 1}}{D_{k,\text{self}}^{x_k \rightarrow 1}}$$

(1) n-hexane / (2) cyclohexane / (3) toluene

	MS Diffusivity/(10 ⁻⁹ m ² s ⁻¹)					
	MD simulation	Prediction of $\mathcal{D}_{ij}^{x_k \rightarrow 1}$				
	\mathcal{D}_{23}	incl. C_x	AD ^a	$C_x = 0$	AD ^a	
$x_1 \rightarrow 1^b$	4.07	4.12	1%	3.78	7%	
$x_2 \rightarrow 1^c$	2.19	2.21	1%	2.69	23%	
$x_3 \rightarrow 1^d$	2.99	2.93	2%	2.82	6%	

^a absolute difference normalized with corresponding value from MD simulations

^b 598 n-hexane molecules; 1 cyclohexane molecule; 1 toluene molecule

^c 1 n-hexane molecule; 598 cyclohexane molecules; 1 toluene molecule

^d 1 n-hexane molecule; 1 cyclohexane molecule; 598 toluene molecules

298K, 1 atm.

(1) ethanol / (2) methanol / (3) water

		$\mathcal{D}_{ij}^{x_k \rightarrow 1} / (10^{-9} \text{ m}^2\text{s}^{-1})$					
	incl. C_x	$C_x = 0$	WK	KT	VKB	DKB	RS
Prediction of \mathcal{D}_{23}	2.68	1.57	2.07	1.25	1.25	1.32	1.61
MD ^b	2.68	2.68	2.68	2.68	2.68	2.68	2.68
AD ^a	0%	41%	23%	53%	53%	51%	40%
Prediction of \mathcal{D}_{13}	3.17	2.07	1.20	2.04	2.04	2.06	1.56
MD ^c	3.24	3.24	3.24	3.24	3.24	3.24	3.24
AD ^a	2%	36%	63%	37%	37%	37%	52%
Prediction of \mathcal{D}_{12}	5.01	1.06	1.78	1.72	1.72	1.73	1.75
MD ^d	4.76	4.76	4.76	4.76	4.76	4.76	4.76
AD ^a	5%	78%	63%	64%	64%	64%	63%

^a absolute difference normalized with corresponding result from MD simulations

^b 168 ethanol molecules; 1 methanol molecule; 1 water molecule

^c 1 ethanol molecule; 248 methanol molecules; 1 water molecule

^d 1 ethanol molecule; 1 methanol molecule; 598 water molecules

298K, 1 atm. Lennard-Jones+electrostatics (Ewald summation)

Consistent multicomponent Darken

Darken equation for a binary system (1945)

$$\mathcal{D}_{ij} = x_i D_{j,\text{self}} + x_j D_{i,\text{self}}$$

Generalized Darken for multicomponent system (empirical)

$$\mathcal{D}_{ij} = \frac{x_i}{x_i + x_j} D_{j,\text{self}} + \frac{x_j}{x_i + x_j} D_{i,\text{self}}$$

Multicomponent Darken (Ind. Eng. Chem. Res., 2011, 50, 10350-10358.)

$$\mathcal{D}_{ij} = D_{i,\text{self}} D_{j,\text{self}} \sum_{i=1}^n \frac{x_i}{D_{i,\text{self}}}$$

- derived by assuming that velocity cross-correlations are much smaller than velocity self-correlations
- for $n = 2$, multicomponent Darken reduces to binary Darken
- for a ternary system for $x_k \rightarrow 1$, our equation for $\mathcal{D}_{ij}^{x_k \rightarrow 1}$ is recovered

Converting Fick and Maxwell-Stefan diffusivities

$$[D_{ij}^{\text{Fick}}] = [B_{ij}]^{-1} [\Gamma_{ij}]$$

$$B_{ii} = \frac{x_i}{\mathcal{D}_{in}} + \sum_{j=1, j \neq i}^n \frac{x_j}{\mathcal{D}_{ij}} \quad \text{with } i = 1, \dots, (n-1)$$

$$B_{ij} = -x_i \left(\frac{1}{\mathcal{D}_{ij}} - \frac{1}{\mathcal{D}_{in}} \right) \quad \text{with } i, j = 1, \dots, (n-1) \quad i \neq j$$

$$\Gamma_{ij} = \delta_{ij} + x_i \left(\frac{\partial \ln \gamma_i}{\partial x_j} \right)_{T,p,\Sigma}$$

Note: molar reference frame for $[D_{ij}^{\text{Fick}}]$

Obtaining Fick diffusivities (1)

$$\left(\frac{\partial \ln \gamma_1}{\partial x_1} \right)_{p,T} = - \frac{c_2 (G_{22} + G_{11} - 2G_{12})}{1 + c_2 x_1 (G_{22} + G_{11} - 2G_{12})}$$

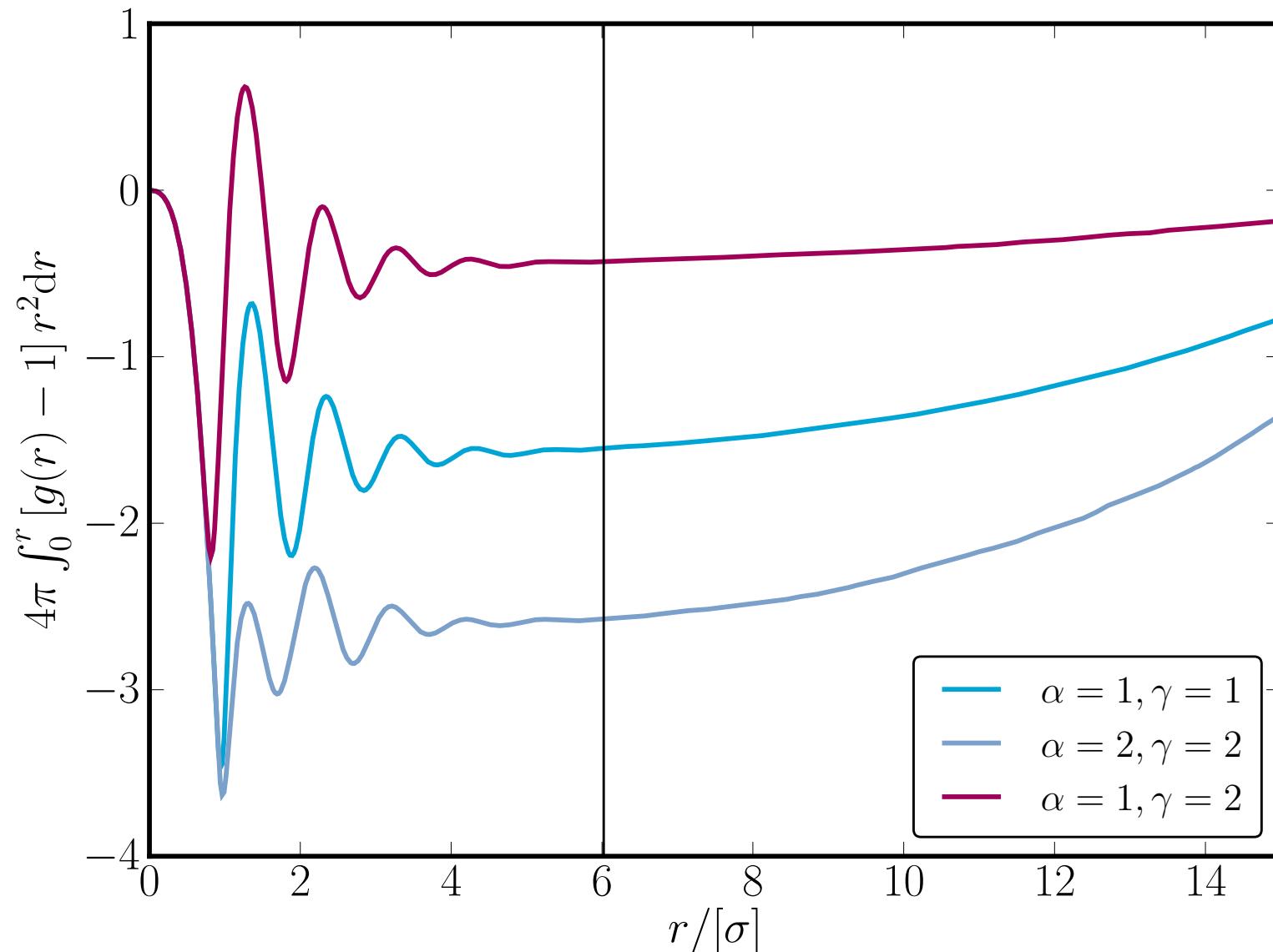
$$\begin{aligned} G_{\alpha\gamma} &= v \frac{\langle N_\alpha N_\gamma \rangle - \langle N_\alpha \rangle \langle N_\gamma \rangle}{\langle N_\alpha \rangle \langle N_\gamma \rangle} - \frac{\delta_{\alpha\gamma}}{c_\alpha} \\ &= 4\pi \int_0^\infty [g_{\alpha\gamma}^{\mu VT}(r) - 1] r^2 dr \\ &\approx 4\pi \int_0^\infty [g_{\alpha\gamma}^{NVT}(r) - 1] r^2 dr \end{aligned}$$

with $c_\alpha = \langle N_\alpha \rangle / v$ and $\langle \dots \rangle$ denotes an average in the μVT ensemble

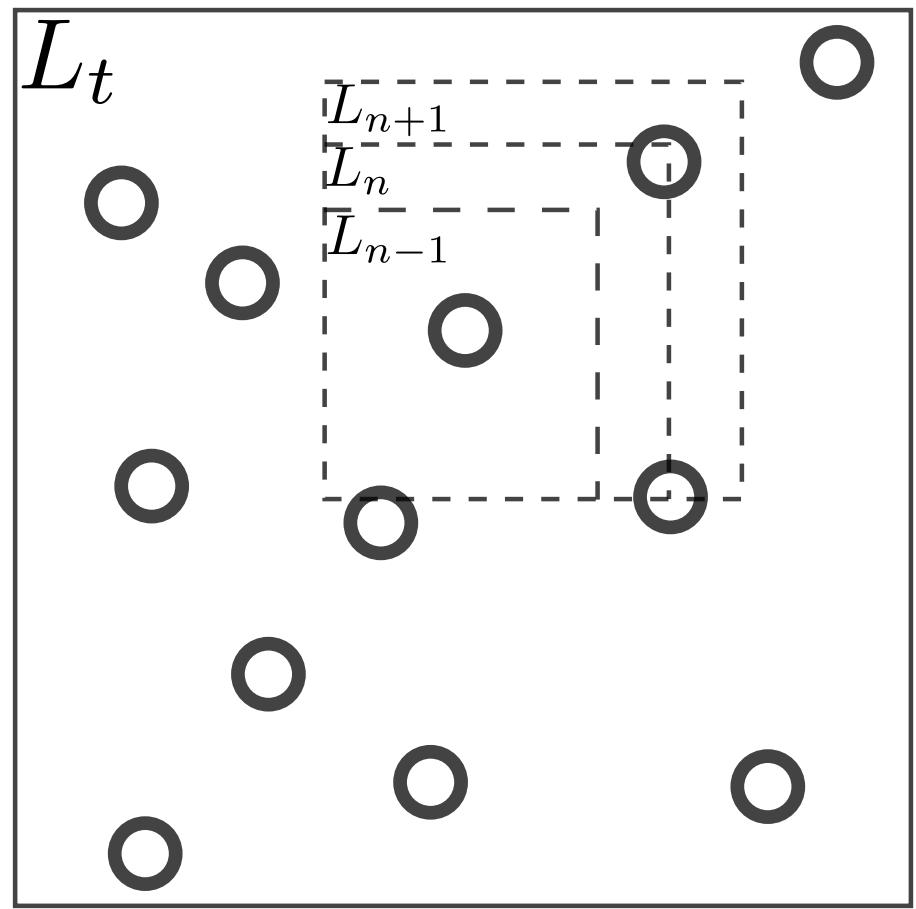
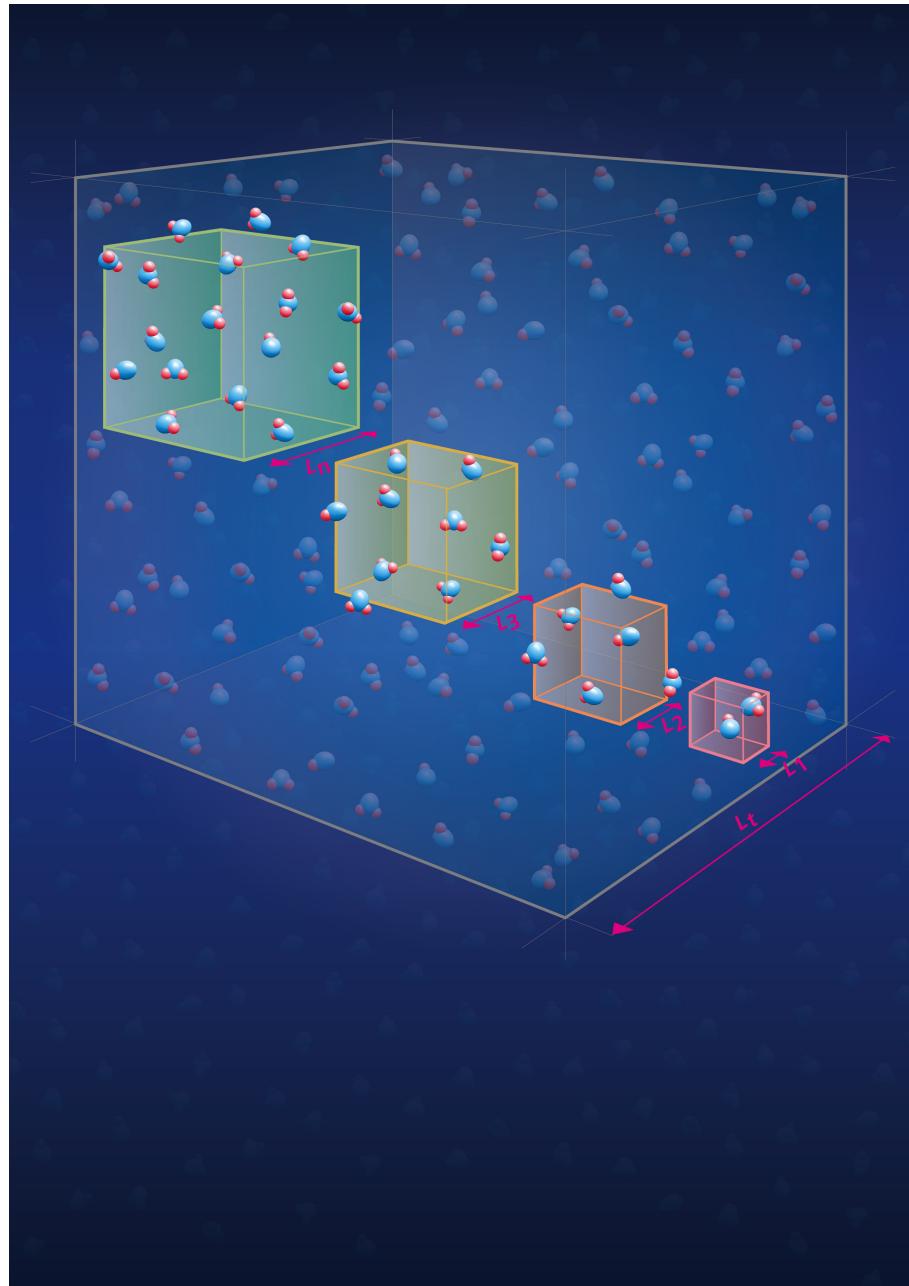
$G_{\alpha\gamma}$: Total Correlation Function Integral (TCFI)

Kirkwood and Buff, J. Chem. Phys., 1951, 19, 774-778.

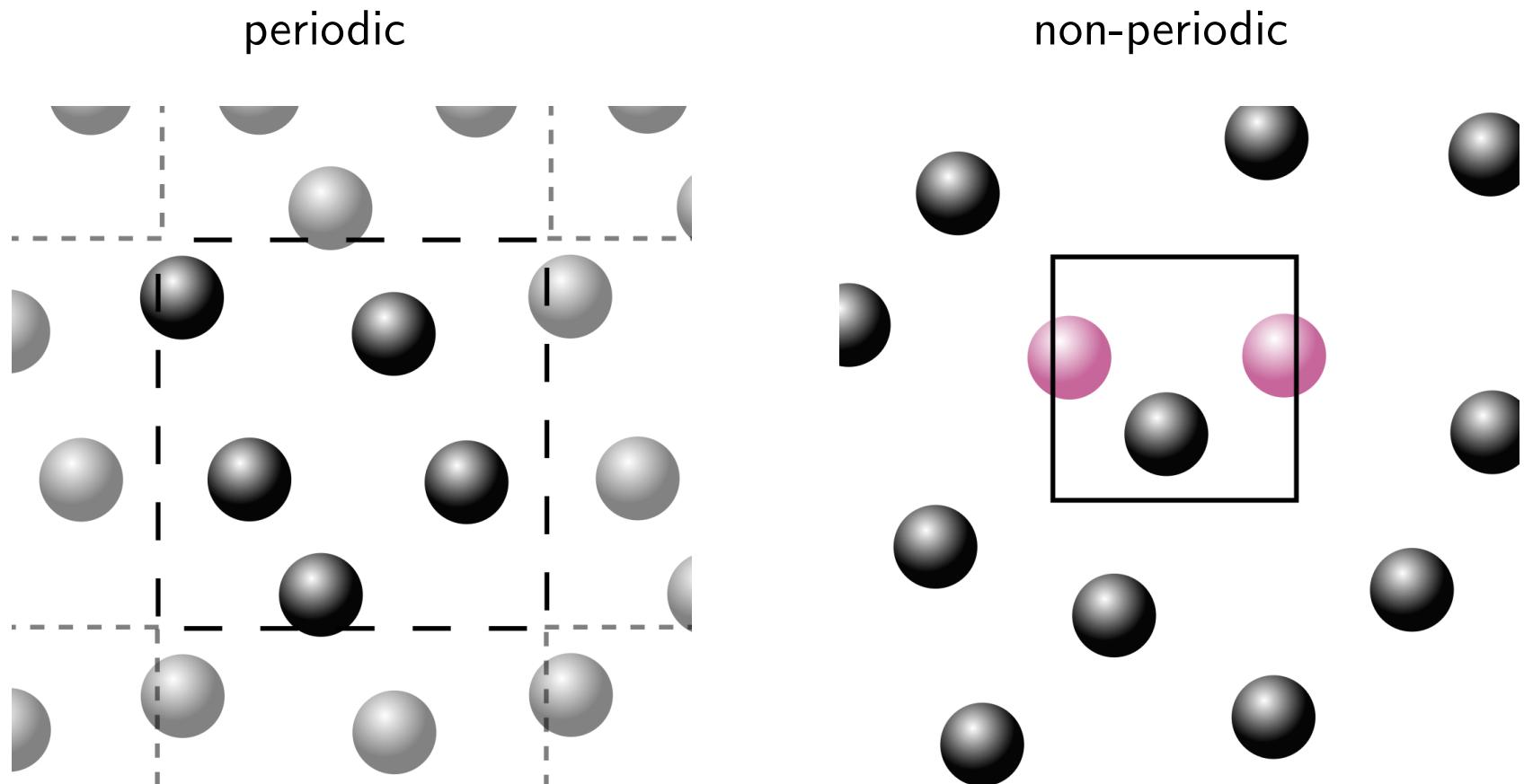
Obtaining Fick diffusivities (2)



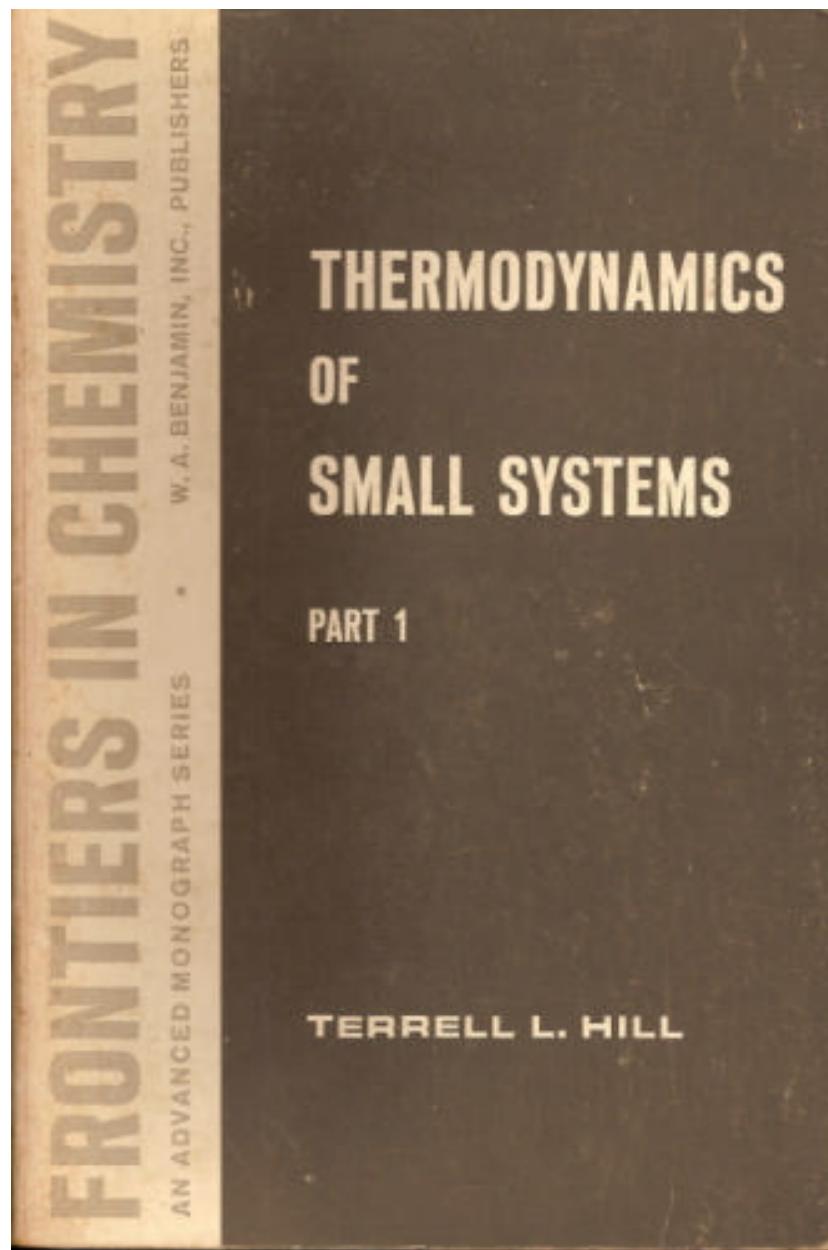
Obtaining Fick diffusivities (3)



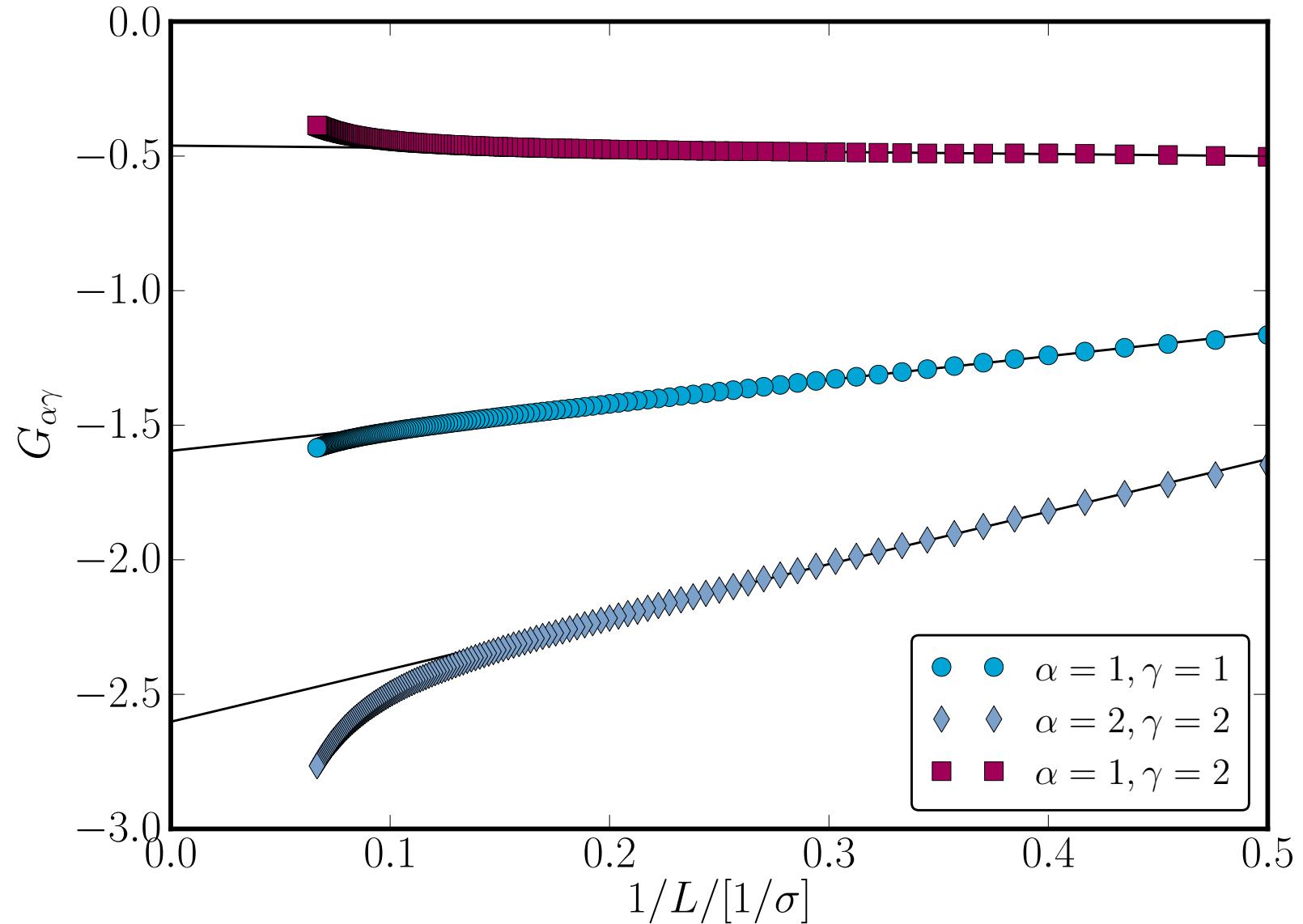
Obtaining Fick diffusivities (4)



Obtaining Fick diffusivities (5)



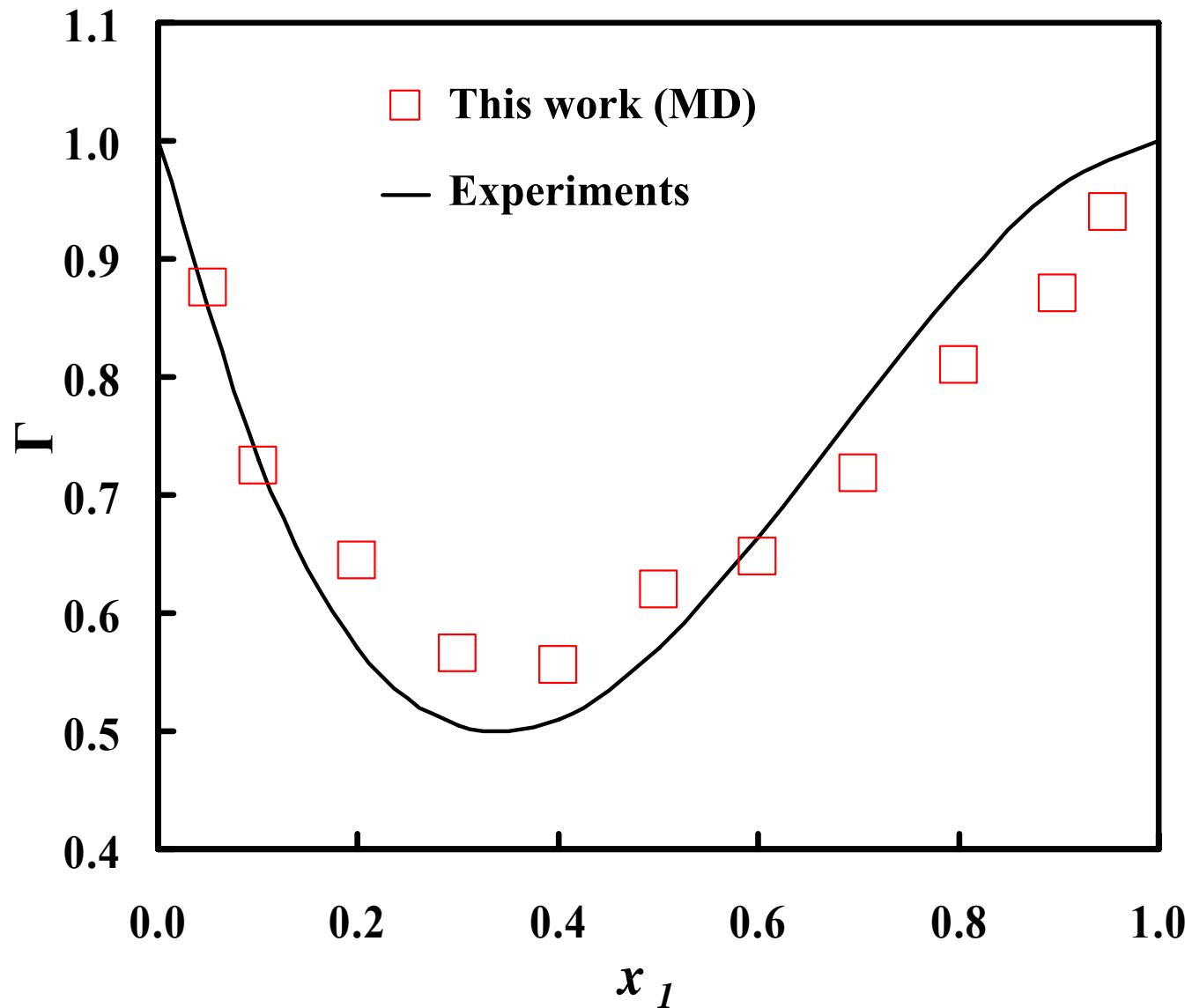
Obtaining Fick diffusivities (6)



Obtaining Fick diffusivities (7)

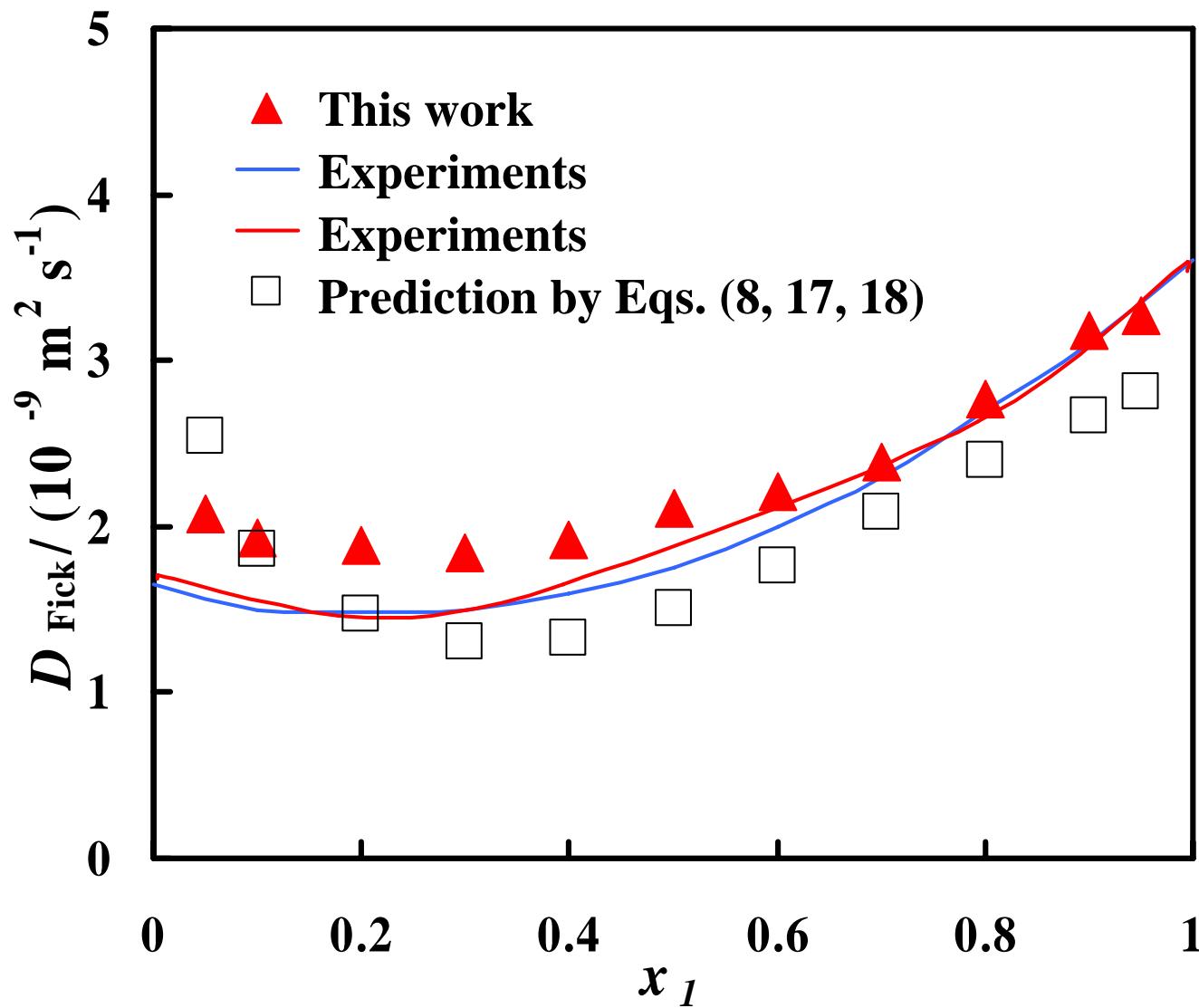
$L_t/[\sigma]$	$\alpha\delta$	$R/[\sigma]$	from $g(r)$	new method
10	11		-0.977	-1.601
	22	4.503	-1.633	-2.686
	12		-0.275	-0.440
20	11		-1.508	-1.594
	22	5.000	-2.456	-2.601
	12		-0.429	-0.464
30	11		-1.552	-1.600
	22	6.023	-2.577	-2.602
	12		-0.428	-0.461
40	11		-1.574	-1.600
	22	6.027	-2.555	-2.621
	12		-0.455	-0.463

Acetone-tetrachloromethane (1)



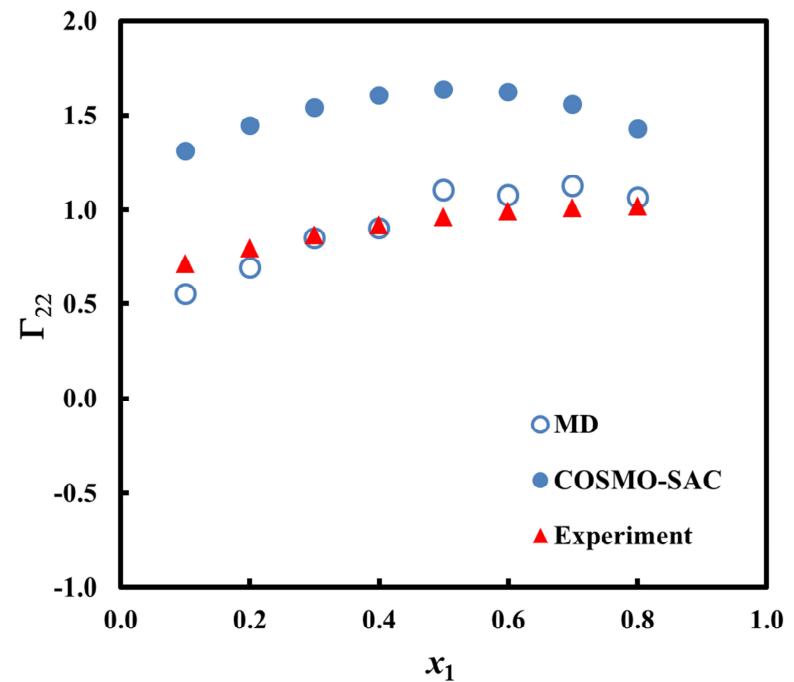
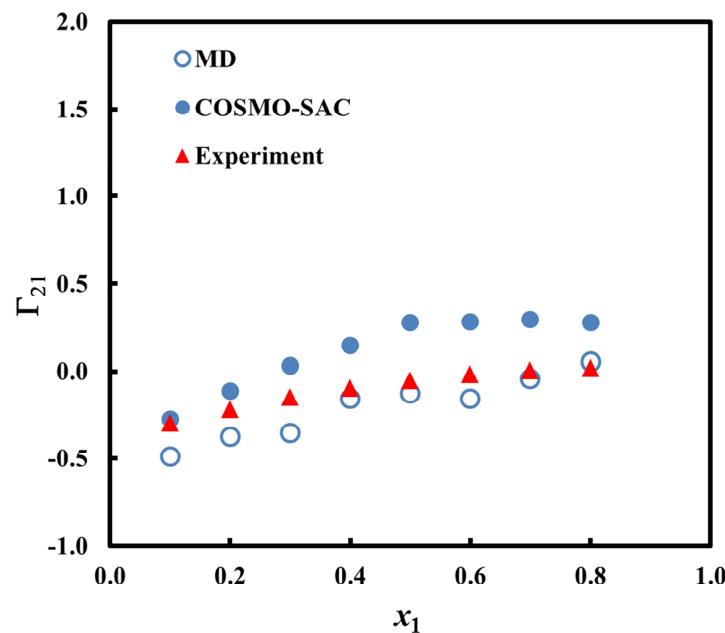
298K, 1atm

Acetone-tetrachloromethane (2)



298K, 1atm

Chloroform(1)-Acetone(2)-Methanol(3) ($x_2 = x_3$)



298K, 1atm

Conclusions

- Transport diffusion coefficients depend on concentration
- Molecular Dynamics and theory are useful tools for developing predictive models for calculating transport diffusivities
- A consistent multicomponent Darken equation was developed
- A new way was found for computing Γ_{ij} from Molecular Dynamics simulations, thereby bridging the gap between experiments and simulations