

# MEASURING LOW VISCOSITIES AND HIGH SHEAR RATES WITH A ROTATIONAL RHEOMETER IN A THIN-GAP PARALLEL-DISK CONFIGURATION

H. DAKHIL<sup>1,2</sup>, A. WIERSCHEM<sup>1\*</sup>

<sup>1</sup>Institute of Fluid Mechanics, Friedrich-Alexander-Universität Erlangen-Nürnberg (FAU),  
91058 Erlangen, Germany

<sup>2</sup>Faculty of Engineering, University of Kufa, Kufa, P.O. Box 21, 00964 Najaf, Iraq

\* Corresponding author: [andreas.wierschem@fau.de](mailto:andreas.wierschem@fau.de)  
Fax: x49.9131.8529503

Received: 4.6.2014, Final version: 6.8.2014

## ABSTRACT:

We modify a commercial rheometer so that the disks are aligned perpendicular to the axis of rotation with a precision in parallelism of about  $1\ \mu\text{m}$  independent of the rheometer reading. This leads to decrease the zero-gap error by a factor of 25 and more. It enables samples to be studied at gap widths well below the absolute error of commercial rheometers. At gap widths of  $20\ \mu\text{m}$ , the modification allows the measurement range to be extended to shear rates up to  $10^5\ \text{s}^{-1}$  enabling to measure low viscosities such as that of solvents or water and of dilute polymer solutions. The measurements are restricted mainly by the torque resolution at low shear rates and by inertia at high shear rates.

## KEY WORDS:

thin-gap rheometry, parallel-disk configuration, low viscous liquids, high shear rates, polymer solutions

## 1 INTRODUCTION

Commercial rotational rheometers are used to measure a wide range of viscosities at shear rates up to about  $10^3\ \text{s}^{-1}$ . Low viscosities may be determined with a double-gap cylindrical system. The parallel-disk configuration is usually employed for higher viscosities at gap widths of about 1 mm. Yet, it has the advantage to select the shear-rate range by adjusting the gap width. At gap widths below about  $100\ \mu\text{m}$ , however, it suffers from errors in determining the zero point. They are caused by viscous resistance to squeeze flow during zeroing and by unevenness and small inclination angles of the plates [1–4]. For the zero-gap error effective values of about  $25\ \mu\text{m}$  or larger have been reported [3, 5, 6]. While the data may be corrected for the zero-gap error, plate inclination and unevenness result in a superposition of elongation flow with the shear flow, which is difficult to access [7]. At low torques, apart from the rheometer resolution, precision is further reduced by contact line forces, which result in a constant torque offset [8]. A value 20 times larger than the manufacturer's specification has been used as a practical low-torque limit [9, 10]. At high shear rates, the measurement range is restricted due to viscous heating, inertial deviations

from viscosimetric flow and radial migration due to centrifugal forces or normal stress differences that may overcome surface tension forces [1, 2, 11–14].

Working at thin gaps offers a number of advantages for commercial rheometers. It extends, for instance, the working range to higher shear rates. Reducing the gap width by about two orders of magnitude increases the maximum shear rate accordingly while thresholds for flow instabilities are shifted to higher shear rates. This enables to carry out measurements at shear rates up to  $10^5\ \text{s}^{-1}$  of viscosities below  $1\ \text{mPa}\cdot\text{s}$ . Also the required amount of sample is drastically reduced, making it attractive for expensive or rare samples. In our setup, about  $40\ \mu\text{l}$  are required at a gap width of  $20\ \mu\text{m}$ . Thin gaps, in principle, also allow for better temperature control at high shear rates. Furthermore, it enables to study the effect of geometrical confinement [15] and the rheology of biological cells [16].

Several groups have built piezoelectric devices to carry out oscillatory studies at gap widths below  $100\ \mu\text{m}$  [17–20]. At small amplitudes frequencies up to the kHz region can be explored. Granick and co-workers developed a shear apparatus for oscillatory studies that works at gap widths down to the sub micrometer range [21, 22]. McKinley and his group reached these gap widths

This is an extract of the complete reprint-pdf, available at the Applied Rheology website  
<http://www.appliedrheology.org>

viscosity function of the aqueous 0.5 wt.% xanthan solution at gap widths of 1000  $\mu\text{m}$ , 100  $\mu\text{m}$  and 20  $\mu\text{m}$ . The open symbols indicate data at a torque below 10  $\mu\text{Nm}$  (at low shear rates) and data at a Reynolds number beyond 10 (at high shear rates). In this case, the Reynolds number was defined with the measured viscosity. For the poly(ethylene oxide) solution, at a gap width of 100  $\mu\text{m}$  this Reynolds number limit is reached at a shear rate below  $10^4 \text{ s}^{-1}$ . Reducing the gap width to 20  $\mu\text{m}$  moves this limit to a shear rate of about  $10^5 \text{ s}^{-1}$ . The minimum shear rate due to the low-torque limit does not depend on the gap width. Yet, as discussed before, at lower shear rates data scatter at 20  $\mu\text{m}$  gap width is larger than at 100  $\mu\text{m}$ .

For the xanthan gum solution, at a gap width of 1000  $\mu\text{m}$  a Reynolds number of 10 is reached at a shear rate below  $10^3 \text{ s}^{-1}$  as shows Figure 4(b). This limit is reached at gap widths of 100  $\mu\text{m}$  and 20  $\mu\text{m}$  at shear rates of about  $10^4 \text{ s}^{-1}$  and  $10^5 \text{ s}^{-1}$ , respectively. The data obtained for different gap widths nicely overlap at high shear rates. At high shear rates strong deviations from the power law is observed and a plateau at high shear rates seems to be reached. Measuring the disk-surface temperature on the gap side after maintaining the shear rate at  $10^4 \text{ s}^{-1}$  for 100 s did not show any deviation from ambient temperature. Increasing the shear rate to  $10^5 \text{ s}^{-1}$  like in Figure 4 resulted in a temperature increase of 0.2 K for the poly(ethylene oxide) and xanthan samples. Finally, we remark that the zero-shear viscosity could not be determined at a gap width of 1000  $\mu\text{m}$  for the poly(ethylene oxide) solution.

#### 4 CONCLUSIONS

We modified a commercial rheometer to align the plates in a parallel-disk configuration perpendicular to the rotational axis. Parallelity is controlled with a precision of about 1  $\mu\text{m}$ . This modification allows to overcome the significant error in the gap height while zeroing the device plates. This enables to measure low viscosities with a parallel-disk configuration. The measurement range is restricted at low shear rates by the torque limit of the rheometer and at high shear rates by inertia. At gap widths of about 20  $\mu\text{m}$ , deviations from viscosimetric flow in thin gaps are shifted to higher shear rates, enabling shear rates to be covered up to about  $10^5 \text{ s}^{-1}$ .

#### ACKNOWLEDGEMENTS

H. D. gratefully acknowledges financial support by Deutscher Akademischer Austauschdienst (DAAD), Germany and the Ministry of Higher Education & Scientific Research, Iraq.

#### REFERENCES

- [1] Connelly RW, Greener J: High-shear viscometry with a rotational parallel-disk device, *J. Rheol.* 29 (1985) 209–226.
- [2] Kramer J, Uhl JT, Prud'Homme RK: Measurement of the viscosity of guar gum solutions to  $50,000 \text{ s}^{-1}$  using a parallel plate rheometer, *Polym. Eng. Sci.* 27(1987) 598–602.
- [3] Davies GA, Stokes JR: On the gap error in parallel plate rheometry that arises from the presence of air when zeroing the gap, *J. Rheol.* 49 (2005) 919–922.
- [4] Andablo-Reyes E, de Vicente J, Hidalgo-Alvarez JR: A method for the estimation of the film thickness and plate tilt angle in thin film misaligned plate-plate rheometry, *J. Non-Newtonian Fluid Mech.* 165 (2010) 882–886.
- [5] Davies GA, Stokes JR: Thin film and high shear rheology of multiphase complex fluids, *J. Non-Newtonian Fluid Mech.* 148 (2008) 73–87.
- [6] Pipe CJ, Majmudar TS, McKinley GH: High shear rate viscometry, *Rheol. Acta* 47 (2008) 621–642.
- [7] Andablo-Reyes E, de Vicente J, Hidalgo-Alvarez, JR: On the nonparallelism effect in thin film plate-plate rheometry, *J. Rheol.* 55 (2011) 981–986.
- [8] Johnston MT, Ewoldt RH: Precision rheometry: Surface tension effects on low-torque measurements in rotational rheometers, *J. Rheol.* 57 (2013) 1515–1532.
- [9] Oliveira MS, Yeh R, McKinley GH: Iterated stretching, extensional rheology and formation of beads-on-a-string in polymer solutions, *J. Non-Newtonian Fluid Mech.* 137 (2006) 137–148.
- [10] Soulages J, Oliveira MS, Sousa PC, Alves MA, McKinley GH: Investigating the stability of viscoelastic stagnation flows in T-shaped microchannels, *J. Non-Newtonian Fluid Mech.* 163 (2009) 9–24.
- [11] Macosko CW: *Rheology: Principles, measurements and applications*, Wiley-VCH (1994).
- [12] Dontula P, Macosko CW, Scriven LE: Does the viscosity of glycerin fall at high shear rates?, *Ind. Eng. Chem. Res.* 38 (1999) 1729–1735.
- [13] Rothstein J, McKinley GH: Non-isothermal modification of purely elastic flow instabilities in torsional flows of polymeric Fluids, *Phys. Fluids* 13 (2001) 382–396.
- [14] Olagunju DO, Cook LP, McKinley GH: Effect of viscous heating on linear stability of viscoelastic cone-and-plate flow: axisymmetric case, *J. Non-Newtonian Fluid Mech.* 102 (2002) 321–342.
- [15] Luengo G, Schmitt FJ, Hill R, Israelachvili J: Thin film rheology and tribology of confined polymer melts: Contrasts with bulk properties, *Macromolecules.* 30 (1997) 2482–2494.

This is an extract of the complete reprint-pdf, available at the Applied Rheology website  
<http://www.appliedrheology.org>

- [16] Fernandez P, Heymann L, Hill R, Ott A, Aksel N, Pullarkat PA: Shear rheology of a cell monolayer, *New J. Phys.* 9 (2007), 419–448.
- [17] Cagnon M, Durand G: Mechanical shear of layers in smectic-A and smectic-B liquid crystal, *Phys. Rev. Lett.* 45 (1980) 1418–1349.
- [18] Fritz G, Pechhold W, Willenbacher N, Wagner NJ: Characterizing complex fluids with high frequency rheology using torsional resonators at multiple frequencies, *J. Rheol.* 47 (2003) 303–319.
- [19] Crassous JJ, Regisser R, Ballauff M, Willenbacher N: Characterization of the viscoelastic behavior of complex fluids using the piezoelastic axial vibrator, *J. Rheol.* 49 (2005) 851–863.
- [20] Roth M, D’Acunzi M, Vollmer D, Auernhammer GK: Viscoelastic rheology of colloid-liquid crystal composites, *J. Chem. Phys.* 132 (2010) 124702.
- [21] Dhinojwala A, Granick S: Micron-gap rheo-optics with parallel plates, *J. Chem. Phys.* 107 (1997) 8664–8667.
- [22] Soga I, Dhinojwala A, Granick S: Optorheological studies of sheared confined fluids with mesoscopic thickness, *Langmuir* 14 (1997) 1156–1161.
- [23] Clasen C, McKinley GH: Gap-dependent microrheometry of complex liquids, *J. Non-Newtonian Fluid Mech.* 124 (2004) 1–10.
- [24] Clasen C, Gearing BP, McKinley GH: The flexure-based microgap rheometer (FMR), *J. Rheol.* 50 (2006) 883–905.
- [25] Clasen C, Kavehpour HP, McKinley GH: Bridging tribology and microrheology of thin films, *App. Rheol.* 20 (2010) 45050.
- [26] Pan L, Arratia PE: A high-shear, low Reynolds number microfluidic rheometer, *Micro. Nano.* 14 (2013) 885–894.
- [27] Pipe CJ, McKinley GH: Microfluidic rheometry, *Mech. Res. Commun.* 36 (2009) 110–120.
- [28] Braithwaite GJ, McKinley GH: Microrheometry for studying the rheology and dynamics of polymers near interfaces, *Appl. Rheol.* 9 (1999) 27–33.
- [29] Anton Paar: Betriebsanleitung UDS 200 universal dynamic spectrometer, Anton Paar (2004).
- [30] Tanner RI, Keentok M: Shear fracture in cone-plate rheometry, *J. Rheol.* 27 (1983) 47–57.

