

# SHEAR RHEOLOGY OF SILICA NANOPARTICLE DISPERSIONS

CIGDEM O. METIN<sup>1</sup>, ROGER T. BONNECAZE<sup>2</sup> AND QUOC P. NGUYEN<sup>1\*</sup>

<sup>1\*</sup> Department of Petroleum and Geosystems Engineering and <sup>2</sup>Department of Chemical Engineering,  
The University of Texas at Austin, 1 University Station, C0300 Austin, TX 78712-1061, USA

\*Corresponding author: [quoc\\_p\\_nguyen@mail.utexas.edu](mailto:quoc_p_nguyen@mail.utexas.edu)  
Fax: x1.512.471.9605

Received: 17.5.2010, Final version: 29.11.2010

## ABSTRACT:

The effects of particle concentration, particle size and temperature on the shear rheology of suspensions of silica nanoparticles are studied. Sterically or electrostatically stabilized silica nanoparticle dispersions with sizes ranging from 5–75 nm and particle volume fractions ranging from 0.22–25 % exhibited a constant viscosity within the shear rate range of 1–200 s<sup>-1</sup>. There is a non-linear relationship between the concentration and the viscosity of these dispersions that depends on the radii and surface energy of these nanoparticles. We propose an effective maximum packing fraction model based on the concept of an effective particle radius, which takes into account the thickness of the electrical double layer and the surface coating material. The viscosities of all the dispersions collapse onto a universal curve as a function of the volume fraction normalized by the effective maximum packing fraction.

## ZUSAMMENFASSUNG:

Der Einfluss der Konzentration und der Größe der Partikel sowie der Temperatur auf die scherrheologischen Eigenschaften von Suspensionen mit Silika-Nanopartikeln wurde untersucht. Sterisch und elektrostatisch stabilisierte Silika-Nanopartikel-Dispersionen mit einer Größe von 5–75 nm und einem Volumenanteil zwischen 0.22% und 25% wiesen eine konstante Scherviskosität im Schergeschwindigkeitsbereich von 1–200 s<sup>-1</sup> auf. Es besteht eine nichtlineare Beziehung zwischen der Konzentration und der Viskosität dieser Dispersionen, die von den Radien und der Oberflächenenergie der Partikel abhängt. Wir stellen ein Modell für die effektive maximale Packungsdichte auf, das auf dem Konzept des effektiven Partikelradius basiert. Dieses Modell berücksichtigt die elektrische Doppelschicht und die Beschichtung der Partikeloberfläche. Die Viskositäten sämtlicher Dispersionen lassen sich als Masterkurve als Funktion des Volumenanteils normiert mit der effektiven maximalen Packungsdichte darstellen.

## RÉSUMÉ:

Les effets de la concentration en particules, de la taille des particules et de la température sur la rhéologie des suspensions de nanoparticules de silice ont été étudiés. Des dispersions de nanoparticules de silice stabilisées au moyen de forces électrostatiques ou stériques, avec des tailles variant de 5 à 75 nm et des fractions volumiques variant de 0.22 à 25%, présentent une viscosité constante pour des vitesses de cisaillement de l'ordre de 1 à 200 s<sup>-1</sup>. Il existe une relation non linéaire entre la concentration de ces dispersions et la viscosité, qui dépend des rayons et de l'énergie de surface des nanoparticules. Nous proposons un modèle de fraction maximum effective de package, basé sur le concept d'un rayon effectif de particule, qui tient compte de l'épaisseur de la double couche électrique et du matériau recouvrant la surface. Les viscosités de toutes les dispersions tombent sur une courbe universelle en fonction de la fraction volumique normalisée para la fraction effective maximum de package.

**KEY WORDS:** silica nanoparticles; particle size; surface coating; effective maximum packing fraction; shear rheology

## 1 INTRODUCTION

The rheological behavior of colloidal dispersions has practical applications to many fields [1]. Recent advances in engineering of nanoparticles have expanded potential application of nanoparticle dispersions into the characterization and production of natural hydrocarbon forma-

tions [2]. Current subsurface technologies are insufficient to measure matrix and fracture properties between wells or to monitor changes in fluid saturation as reservoir pressure changes with respect to hydrocarbon production. An improved understanding of spatial distribution of fluids in the reservoir and their properties

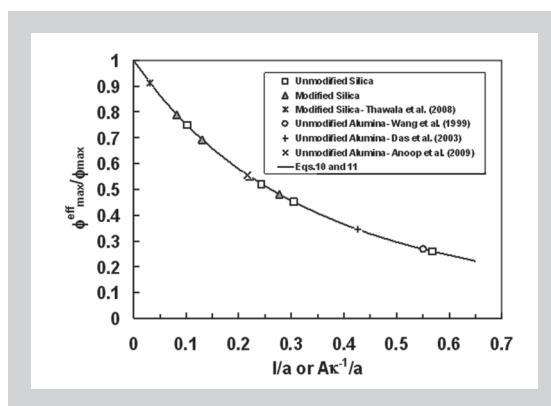
© Appl. Rheol. 21 (2011) 13146

DOI: 10.3933/ApplRheol-21-13146

This is an extract of the complete reprint-pdf, available at the Applied Rheology website

<http://www.appliedrheology.org>

**Figure 9 (left):**  
The normalized effective maximum packing fraction with respect to maximum packing fraction,  $\phi_{\text{eff max}}/\phi_{\text{max}}$ , as a function of dimensionless parameter  $l/a$  for modified surface and  $A\kappa^{-1}/a$  for unmodified surface. The solid line is constructed using Equations 10 and 11.



**Figure 10:**  
Viscosity ratio as a function of volume fraction of alumina nanoparticles in dispersed in water [13, 14, 40] and MEG coated silica nanoparticle dispersions [30]. The effective maximum volume fractions are determined by Equations 9–11. All the data collapse onto a single curve that is well represented by our unified model.

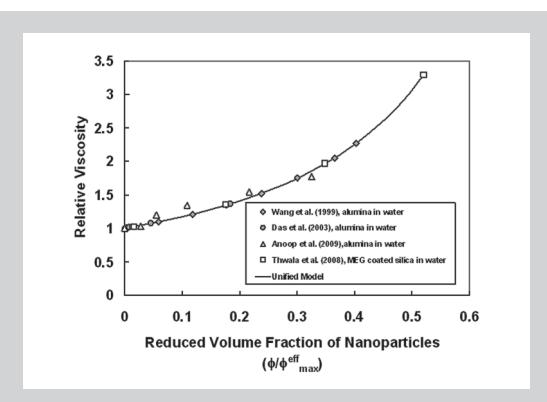
for surface modified and  $A\kappa^{-1}/a$  for unmodified silica particles. The nonlinear dependence of  $\phi_{\text{eff max}}/\phi_{\text{max}}$  on dimensionless length described by Eqs. 10 and 11 is shown in Figure 9. The relationship between  $\phi_{\text{eff max}}/\phi_{\text{max}}$  and  $A\kappa^{-1}/a$  or  $l/a$  indicates a significant deviation of  $\phi_{\text{eff max}}$  from  $\phi_{\text{max}}$  (0.63) especially at small particle sizes (Figure 9).

We used our viscosity model (Equations 9–10/11) to predict the measured viscosity of alumina and silica dispersions at different volume fractions and sizes from [13, 14, 30, 40]. The particle sizes reported in these references were used to determine the corresponding model parameters ( $A$  or  $l$ ) based on Figure 8. These model parameters were then used to calculate the viscosity (Equations 9 – 10/11). We assumed a double layer thickness of 5 nm since the information on the electrical double layer thickness was not given in these studies. All the calculated viscosities and their measured values from the references were plotted versus particle volume fraction in Figure 10. The relative viscosities of these dispersions collapse onto a single curve (Figure 10) as represented by the unified model (Equations 9 – 11).

#### 4 CONCLUSIONS

In this study we have shown that silica nanoparticle dispersions exhibit a Newtonian behavior for shear rates ranging from 1 – 200 s<sup>-1</sup> and particle concentrations ranging from 0.22 – 25 % by volume. The relative viscosity is a non-linear function of particle volume fraction and independent of temperature. The particle size and the surface type are also found to significantly influence the viscosity. The dispersion viscosity increases as particle size decreases. The unmodified, electrostatically stabilized silica nanoparticles exhibit greater viscosity than sulfonate coated, sterically stabilized silica nanoparticles at a given particle size and volume fraction.

A significant deviation from the predictions of hard sphere viscosity model occurs with our experimental results. Therefore, the electrostatic or steric interactions between silica nanoparticles should be taken into account. We propose a unified model to predict accurately the viscosity



of silica nanoparticle dispersions at a given solid volume fraction by introducing the concept of effective maximum packing fraction. The model parameters ( $A$  or  $l$ ) could be determined experimentally or numerically based on, for instance molecular dynamics simulation. These parameters depend on nanoparticle size and surface properties. All the experimental data are successfully scaled by normalizing the volume fraction by the effective maximum packing fraction. A correlation is obtained between the effective maximum packing fraction and particle radius.

#### REFERENCES

- [1] Mokhatab S, Fresky MA, Islam MR: Applications of nanotechnology in oil and gas E&P, J. Pet. Technol. Online 58 (2006) 4.
- [2] Nanotechnology for oil and gas operations, <http://www.offshore-mag.com/index/article-tools-template.articles.offshore.regional-reports.north-sea-northwest-europe.2009.09.nanotechnology-shows.html>
- [3] Prodanovic M, Ryoo S, Rahmani AR, Kuranov R, Kotzmar C, Milner TE, Johnston KP, Bryant SL, Huh C: Effects of magnetic field on the motion of multiphase fluids containing paramagnetic nanoparticles in porous media, SPE 129850, SPE IOR Symp. (2010).
- [4] Moon T: Nanotechnology collaborative takes aim at EOR, JPT online (2008). <http://www.spe.org/jpt/2008/12/nanotechnology-collaborative-takes-aim-at-eor/#more-1870>.
- [5] Namburu PK, Kulkarni DP, Dandekar A, Das DK: Experimental investigation of viscosity and specific heat of silicon dioxide nanofluids, Micro & Nano Lett. 2 (2007) 67-71.
- [6] Russel WB, Saville DA, Schowalter WR: Colloidal dispersions, Cambridge University Press, Cambridge (1991).
- [7] Chow TS: Viscosities of concentrated dispersions, Phys. Rev. E 48 (1993) 1977-1983.
- [8] Petrie CJS: The rheology of fiber suspensions, J. Non-Newtonian Fluid Mech. 87 (1999) 369-402.
- [9] Larson RG: The rheology of dilute solutions of flexible polymers: Progress and problems, J. Rheology 49 (2005) 1-70.
- [10] Bergenholtz J: Theory of rheology of colloidal dispersions, Current Opinion Colloid Int. Sci. 6 (2001) 484-488.

- [11] Stickel JJ, Powell RL: Fluid mechanics and rheology of dense suspensions, *Ann. Rev. Fluid Mech.* 37 (2005) 129-149.
- [12] Choi SUS: Enhancing thermal conductivity of fluids with nanoparticles, in *Developments and applications of non-Newtonian flows*, Signer DA and Wang HP (Eds), FED-Vol 231/MD-Vol 66, ASME, New York (1995) 99-105.
- [13] Das SK, Putra N, Roetzel W: Pool boiling characteristics of nano-fluids, *Int. J. Heat Mass Transfer* 46 (2003) 851-862.
- [14] Wang XW, Xu XF, Choi SUS: Thermal conductivity of nanoparticle-Fluid Mixture, *J. Thermophys. Heat Transfer* 13 (1999) 474-480.
- [15] Xuan YM, Li Q: Heat transfer enhancement of nanofluids, *Int. J. Heat Fluid Flow* 21 (2000) 58-64.
- [16] Prasher R, Song D, Wang J, Phelan P: Measurements of nanofluid viscosity and its implications for thermal applications, *Appl. Phys. Lett.* 89 (2006) 133108.
- [17] Ding YL, Alias H, Wen DS, Williams RA: Heat transfer of aqueous suspensions of carbon nanotubes (CNT nanofluids), *Int. J. Heat and Mass Transfer* 49 (2006) 240-250.
- [18] Ma AWK, Chinesta F, Mackley MR, Ammar A: The rheological modeling of carbon nanotube (CNT) suspensions in steady shear flow, *Int. J. Mater. Form.* 1 (2008) 83-88.
- [19] He Y, Jin Y, Chen H, Ding Y, Cang D, Lu H: Heat transfer and flow behaviour of aqueous suspensions of TiO<sub>2</sub> nanoparticles (nanofluids) flowing upward through a vertical pipe, *Int. J. Heat and Mass Transfer* 50 (2007) 2272-2281.
- [20] Tseng WJ, Lin KC: Rheology and colloidal structure of aqueous TiO<sub>2</sub> nanoparticle suspensions, *Mater. Sci. Eng. A* 355 (2003) 186-192.
- [21] Kwak K, Kim C: Viscosity and thermal conductivity of copper oxide nanofluid dispersed in ethylene glycol, *Korea-Australia Rheol. J.* 17 (2005) 35-40.
- [22] Studart AR, Amstad E, Antoni M, Gauckler LJ: Rheology of concentrated suspensions containing weakly attractive alumina nanoparticles, *J. Am. Ceram. Soc.* 89 (2006) 2418-25.
- [23] Jung K-M, Kim SH: Rheological properties and transfer phenomena of nanofluids, XV<sup>th</sup> International Congress on Rheology/The Society of Rheology 80<sup>th</sup> Annual Meeting (2008) 773-775.
- [24] Lu K, Kessler C: Colloidal dispersion and rheology study of nanoparticles, *J. Mater. Sci.* 41 (2006) 5613-5618.
- [25] McPhie MG, Daivis PJ, Snook IK: Viscosity of a binary mixture: Approach to the hydrodynamic limit, *Phys. Rev. E* 74 (2006) 031201.
- [26] Rudyak VYa, Belkin AA, Egorov VV: Effective viscosity coefficient of nanosuspensions, *Rarefied Gas Dynamics, 26<sup>th</sup> International Symposium, Amer. Inst. Phys.* (2009) 489-494.
- [27] Liu SF, Lafuma F, Audebert R: Rheological behavior of moderately concentrated silica suspensions in the presence of adsorbed poly(ethylene oxide), *Colloid Polym. Sci.* 272 (1994) 196-203.
- [28] Fagan ME, Zukoski CF: The rheology of charge stabilized silica suspensions, *J. Rheol.* 41 (1997) 373-397.
- [29] Chevalier J, Tillement O, Ayela F: Rheological properties of nanofluids flowing through micro-channels, *App. Phys. Lett.* 91 (2007) 233103.
- [30] Thwala JM, Goodwin JW, Mills PD: Viscoelastic and shear viscosity studies of colloidal silica particles dispersed in monoethylene glycol (MEG), diethylene Glycol (DEG) and dodecane stabilized by dodecyl hexaethylene glycol monoether, *Langmuir* 24 (2008) 12858-12866.
- [31] Starck P, Mosse WKJ, Nicholas NJ, Spiniello M, Tyrrell J, Nelson A, Qiao GG, Ducker WA: Surface chemistry and rheology of polysulfobetaine-coated silica, *Langmuir* 23 (2007) 7587-7593.
- [32] Lake LW: Enhanced oil recovery, Prentice Hall, New Jersey (1989).
- [33] Einstein A: Investigations on the theory of the Brownian movement, Dover, New York (1956).
- [34] Mooney M: The viscosity of a concentrated suspension of spherical particles, *J. Colloid Sci.* 6 (1951) 162-170.
- [35] Chong JS, Christiansen EB, Baer AD: Rheology of concentrated suspensions, *J. Appl. Polym. Sci.* 15 (1971) 2007-2021.
- [36] Thomas DG: Transport characteristics of suspension: VIII. A note on the viscosity of Newtonian suspensions of uniform spherical particles, *J. Colloid Sci.* 20 (1965) 267-277.
- [37] Fedors RF: Relations between viscosity and concentration for Newtonian suspensions, *J. Colloid Interface Sci.* 46 (1974) 545-547.
- [38] Krieger IM, Dougherty RJ: A mechanism for non-Newtonian flow in suspensions of rigid spheres, *Trans. Soc. Rheol.* 3 (1959) 137-152.
- [39] Murshed SMS, Tan S-H, Nguyen N-T: Temperature dependence of interfacial properties and viscosity of nanofluids for droplet-based microfluidics, *J. Phys. D: Appl. Phys.* 41 (2008) 085502.
- [40] Mackay ME, Dao TT, Tuteja A, Ho DL, Van Horn B, Kim H-C, Hawker CJ: Nanoscale effects leading to non-Einstein-like decrease in viscosity, *Nature Materials* 2 (2003) 762-766.
- [41] Anoop KB, Kabelac A, Sundararajan T, Das SK: Rheological and flow characteristics of nanofluids: Influence of electroviscous effects and particle agglomeration, *J. App. Phys.* 106 (2009) 034909.
- [42] Roberts WO: *Colloidal Silica: Fundamentals and Applications*, Bergna HE, Roberts WO (Eds.), CRC Press, Boca Raton (2006).



This is an extract of the complete reprint-pdf, available at the Applied Rheology website  
<http://www.appliedrheology.org>

This is an extract of the complete reprint-pdf, available at the Applied Rheology website  
<http://www.appliedrheology.org>

Applied Rheology  
 Volume 21 · Issue 1

13146-8