

BUBBLE RISE VELOCITY AND TRAJECTORY IN XANTHAN GUM CRYSTAL SUSPENSION

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ABSTRACT:

An experimental set-up was used to visually observe the characteristics of bubbles as they moved up a column holding xanthan gum crystal suspensions. The bubble rise characteristics in xanthan gum solutions with crystal suspension are presented in this paper. The suspensions were made by using different concentrations of xanthan gum solutions with 0.23 mm mean diameter polystyrene crystal particles. The influence of the dimensionless quantities; namely the Reynolds number, Re , the Weber number, We , and the drag co-efficient, c_d , are identified for the determination of the bubble rise velocity. The effect of these dimensionless groups together with the Eötvös number, Eo , the Froude number, Fr , and the bubble deformation parameter, D , on the bubble rise velocity and bubble trajectory are analysed. The experimental results show that the average bubble velocity increases with the increase in bubble volume for xanthan gum crystal suspensions. At high We , Eo and Re , bubbles are spherical-capped and their velocities are found to be very high. At low We and Eo , the surface tension force is significant compared to the inertia force. The viscous forces were shown to have no substantial effect on the bubble rise velocity for $45 < Re < 299$. The results show that the drag co-efficient decreases with the increase in bubble velocity and Re . The trajectory analysis showed that small bubbles followed a zigzag motion while larger bubbles followed a spiral motion. The smaller bubbles experienced less horizontal motion in crystal suspended xanthan gum solutions while larger bubbles exhibited a greater degree of spiral motion than those seen in the previous studies on the bubble rise in xanthan gum solutions without crystal.

ZUSAMMENFASSUNG:

Ein experimenteller Aufbau wurde verwendet, um die Eigenschaften von Blasen bei ihrer Strömung durch eine Kolonne mit einer Suspension aus Xanthangummi und Kristallen visuell zu beobachten. Die Eigenschaften der aufsteigenden Blasen in der Xanthangummilösung mit suspendierten Kristallen werden in diesem Artikel vorgestellt. Die Suspensionen von Xanthangummilösungen mit Polystyrolkristallen, die einen mittleren Durchmesser von 0.23 mm besitzen, wurden mit unterschiedlichen Konzentrationen hergestellt. Der Einfluss dimensionsloser Größen, d. h. der Reynoldszahl Re , der Weberzahl We und des Drag-Koeffizienten c_d wird bei der Bestimmung der Aufstiegs geschwindigkeit der Bläschen erläutert. Der Einfluss dieser dimensionslosen Gruppe zusammen mit der Eötvös-Zahl Eo der Froude-Zahl Fr und des Blasendeformationsparameters D auf die Aufstiegsgeschwindigkeit der Blasen und die Trajektorien der Blasen wird analysiert. Die experimentellen Resultate zeigen, dass die mittlere Blasengeschwindigkeit mit dem Blasenvolumen für Xanthangummikristallsuspensionen zunimmt. Bei hohen Werten von We , Eo und Re besitzen die Blasen eine kugelförmige Gestalt und eine hohe Geschwindigkeit. Bei niedrigen We , Eo und Re ist die Oberflächenspannung groß im Vergleich zu den Trägheitskräften. Die viskosen Kräfte haben keinen signifikanten Einfluss auf die Aufstiegsgeschwindigkeit der Blasen für $45 < Re < 299$. Die Ergebnisse zeigen, dass der Drag-Koeffizient mit der Blasengeschwindigkeit und mit Re abnimmt. Die Analyse der Trajektorien belegt, dass kleinere Blasen eine Zigzag-Bewegung durchführen, während sich größere Blasen spiralförmig bewegen. Die kleineren Blasen führen eine geringere horizontale Bewegung in mit Kristallen suspendierten Xanthangummilösungen durch, während größere Blasen eine stärkere spiralförmige Bewegung aufweisen als sie in vorherigen Studien mit Xanthangummilösungen ohne Kristalle beobachtet worden ist.

RÉSUMÉ:

Un dispositif expérimental a été utilisé pour observer visuellement les caractéristiques des bulles en se déplaçant d'une colonne contenant la gomme de xanthane suspensions de cristal. Les caractéristiques de montée des bulles dans les solutions de gomme xanthane avec la suspension de cristal sont présentés dans le présent document.

inertia forces had a strong influence on the bubble rise velocity. However, for the larger bubbles investigated (high We and Re), inertia forces governed the bubble rise velocity, and surface tension and viscous forces were shown to be less important. The effect of Fr on bubble rise velocity was found to be insignificant for the range of conditions studied. The results also showed that, as the Re increased, the drag co-efficient decreased resulting in increases in bubble rise velocity.

The trajectory results were able to demonstrate common trends for the different bubble sizes. The trajectory analysis showed small bubbles experienced less horizontal motion in crystal suspended xanthan gum solutions in comparison with the bubble rise in xanthan gum solution without crystal. This is due to the presence of crystal in xanthan gum solution which increased the solution viscosity. Larger bubbles produced more spiral motion in crystal suspended xanthan gum solutions as larger bubble experience more resistance on top and deform as their size increases. At low We and Re for smaller bubbles, the rising bubbles showed a zigzag trajectory, while larger bubbles at high We and Re exhibited spiral motion. The zigzag motion occurs due to an interaction between the instability of the straight trajectory and that of the wake produced by vortices. The results of this study have given important information and data of the entire flow characteristics of bubbles which could be used to develop a CFD model. This innovative predicted model can be used to gain a sound knowledge of mass and heat transfer operations in vacuum pans used in sugar mills.

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REFERENCES

- [1] Broadfoot R, Miller KF, McLaughlin RL: Rheology of High Grade Massecuites, Proc. Aust. Soc. Sugar Cane Technol. 20 (1998) 388–397.
- [2] Rackemann DW: Evaluation of Circulation and Heat Transfer in Calandria Tubes of Crystallisation Vacuum Pans, MSc. Eng. Thesis, 2005, James Cook University.
- [3] Ness JN: On the Measurement of Massecuite Flow Properties, Proc. Int. Soc. Sugar Cane Technol. 18 (1983) 1295–1303.
- [4] Broadfoot R, Miller KF: Rheological Studies of Massecuites and Molasses, International Sugar Journal 92 (1990) 1098.
- [5] Awang M, White ET: Effect of Crystal on the Viscosity of Massecuites, Proc. Qld Soc. Sugar Cane Technol. 43 (1976) 263–270.
- [6] Adkins BG: Notes on the viscosity of molasses and massecuites, Proc. Qld Soc. Sugar Cane Technol. 18 (1951) 43–52.
- [7] Nezhad Hazi A: Materials Science Experimentations of Raw Materials, Intermediates and Final Products in the Sugar Beet manufacturing Process, PhD-Thesis, Technical University of Berlin (2008).
- [8] Kulkarni AA, Joshi JB: Bubble Formation and Bubble Rise Velocity in Gas-Liquid Systems: A Review, Ind. Eng. Chem. Res. 44 (2005).
- [9] Shew WL, Pinton JF: Viscoelastic Effects on the Dynamics of a Rising Bubble, J. Stat. Mech. (2006) doi: 10.1088/1742-5468/2006/01/P01009
- [10] Wu M, Gharib M: Experimental Studies on the Shape and Path of Small Air Bubbles Rising in Clean Water, Phys. Fluids 14 (2002) 7.
- [11] Saffman PG: On the Rise of Small Air Bubbles in Water. J. Fluid Mech. 1 (1956) 249–275.
- [12] Hassan NMS, Khan MMK, Rasul MG, Rackemann DW: An Experimental Study of Bubble Rise Characteristics in Non-Newtonian (Power-Law) Fluids, Proceedings of the 16th Australasian Fluid Mechanics Conference, Gold Coast, Australia (2007) 1315–1320.
- [13] de Vries AWG, Biesheuvel A, van Wijngaarden L: Notes on the Path and Wake of a Gas Bubble Rising in Pure Water, Int. J. Multiphase Flow 28 (2002) 1823.
- [14] Mougin G, Magnaudet J: Path instability of a rising bubble, Phys. Rev. Lett. 88 (2002) 014502.
- [15] Feng ZC, Leal, LG: Nonlinear Bubble Dynamics, Ann. Rev. Fluid Mech. 29 (1997) 201–243.
- [16] Yoshida S, Manasseh R: Trajectories of rising bubbles, 16th Japanese Multiphase Flow Symposium, Touha, Japan (1997).
- [17] Shew WL, Pinton JF: Dynamical Model of Bubble Path Instability, Phys. Rev. Lett. 97 (2006) 144508.
- [18] Dewsbury K, Karamanov DG, Margaritis A: Hydrodynamic Characteristics of free Rise of Light solid Particles and Gas Bubbles in Non-Newtonian Liquids, Chem. Eng. Sci. 54 (1999) 4825–4830.
- [19] Tsuge H, Hibino SI: The Onset conditions of Oscillatory Motion of Single Gas Bubbles Rising in various Liquids, J. Chem. Eng. Japan 10 (1997) 66–68.
- [20] Margaritis A, te Bokkel DW, Karamanov DG: Bubble Rise Velocities and Drag Coefficients in Non-

- Newtonian Polysaccharide Solutions, John Wiley & Sons Inc (1999).
- [21] Belmonte A: Self-oscillations of a Cusped Bubble Rising through a Micellar Solution, *Rheol. Acta* 39 (2000) 554–559.
- [22] Chhabra RP: Bubbles, Drops, and Particles in Non-Newtonian Fluids, Taylor & Francis Group, CRC Press (2006).
- [23] Astarita G, Apuzzo G: Motion of Gas Bubbles in Non-Newtonian Liquids, *AIChE J.* 11 (1965) 815–820.
- [24] Acharya A, Mashelkar RA, Ulbrecht J: Mechanics of Bubble Motion and Deformation in non Newtonian Media, *Chem. Eng. Sci.* 32 (1977) 863–872.
- [25] Calderbank PH, Johnson DSL, Loudon J: Mechanics and Mass Transfer of Single Bubbles in Free Rise through some Newtonian and Non-Newtonian Liquids, *Chemical Engineering Science*, 25 (1970) 235–256.
- [26] De Kee D, Carreau PJ, Mordarski J: Bubble Velocity and Coalescence in Viscoelastic Liquids, *Chem. Eng. Sci.* 41 (1986) 2273–2283.
- [27] De Kee D, Chhabra RP, Dajan A: Motion and Coalescence of Gas Bubbles in Non Newtonian Polymer Solutions, *J. Non-Newtonian Fluid Mech.* 37 (1990) 1–18.
- [28] Haque MW, Nigam KDP, Viswanathan K, Joshi JB: Studies on Bubble Rise Velocity in Bubble Columns Employing Non-Newtonian Solutions, *Chem. Eng. Comm.* 73 (1988) 31–42.
- [29] Abou-EL-Hassan ME: Generalized Bubble Rise Velocity Correlation, *Chem. Eng. Commun.* 22 (1982) 243–250.
- [30] Clift R, Grace JR, Weber ME: Bubbles, Drops and Particles, Academic Press (1978).
- [31] Brennen CE: Fundamentals of Multiphase Flow, Cambridge University Press (2005).
- [32] Churchill SW: A Theoretical Structure and Correlating Equation for the Motion of Single Bubbles, *Chem. Eng. Process* 26 (1989) 269–279.
- [33] Haberman WL, Morton RK: An Experimental Study of Bubbles Moving in Liquids, *Trans. ASCE* 2799 (1954) 227–252.
- [34] Hartunian RA, Sears WR: On the Instability of Small Gas Bubbles Moving Uniformly in Various Liquids, *J. Fluid Mech.* 378 (1957) 19–70.
- [35] Aybers NM, Tapucu A: The Motion of Gas Bubble Rising through Stagnant Liquid, *Wärme und Stoffübertragung* 2 (1969) 118–128.
- [36] Duineveld PC: The Rise Velocity and Shape of Bubbles in Pure Water at high Reynolds number, *J. Fluid Mech.* 292 (1995) 325–332.
- [37] Deane GB, Stokes MD: Scale Dependence of Bubble Creation Mechanisms in Breaking Waves, *Nature* 418 (2002) 839–844.
- [38] Whyte DS, Davidson MR, Carnie S, Rudman, MJ: Calculation of Droplet Deformation at Intermediate Reynolds Number using a Volume of Fluid Technique, *ANZIAM J.* 42 (2000) C1520–C1535.
- [39] Lali AM, Khare AS, Joshi JB, Nigam KDP: Behaviour of Solid Particles in Viscous Non-Newtonian Solutions: Settling Velocity, Wall Effects and Bed Expansion in Solid-Liquid Fluidized Beds, *Powder Technol.* 57 (1989) 39–50.
- [40] Dewsbury K, Karamanov DG, Margaritis A: Dynamic Behaviour of Freely Rising Buoyant Solid Spheres in Non-Newtonian Liquids, *AIChE J.* 46 (2000) 46–51.
- [41] Miyhara T, Takahashi T: Drag Coefficient of a Single Bubble Rising through a Quiescent Liquid, *Inter. Chem. Eng.* 26 (1985) 146–148.
- [42] Lima-Ochoterena R, Zenit R: Visualization of the Flow around a Bubble Moving in a Low Viscosity Liquid, *Revista Mexicana De Fisica* 49 (2003) 348–352.
- [43] Paday JF: Surface tension. Part III: Tables relating the size and shape of liquid drops to the surface tension. In Matijevic E (Ed), *Surface and colloid science*. New York: Wiley-Interscience (1969) 151–197.
- [44] Doiz M, Corrias F, Diez-Sales O, Casanova A, Hernandez, MJ: Influence of test times on creep and recovery behaviour of Xanthan gum hydrogels, *Appl. Rheol.* 19 (2009) 34201.
- [45] Kabir MA, Slater AR, Khan MMK, Rackemann D, Characteristics of Bubble Rise in Water and Polyacrylamide Solutions, *Inter. J. Mecha. Mater. Eng.* 1 (2006) 64–69.
- [46] Davies RM, Taylor GI: The mechanics of large bubbles rising through liquids in tubes, *Proc. Roy. Soc. London A* 200 (1950) 375–390.
- [47] Turton R, Levenspiel O: A short note on the drag correlation for spheres, *Powder Technol.* 4 (1986) 83–86.
- [48] Khan AR, Richardson JF: The resistance to motion of a solid sphere in a fluid, *Chem. Eng. Commun.* 62 (1987) 135–150.
- [49] Hassan NMS, Khan MMK, Rasul MG: Characteristics of Air Bubble Rising in Low Concentration Polymer Solutions, *WSEAS Trans. Fluid Mech.* 2 (2007) 53–60.
- [50] Hassan NMS, Khan MMK, Rasul MG: An Investigation of Bubble Trajectory and Drag Co-efficient in Water and Non-Newtonian Fluids, *WSEAS Trans. Fluid Mech.* 3 (2008) 261–270.
- [51] De Kee D, Chhabra RP: A Photographic Study of Shapes of Bubbles and Coalescence in non-Newtonian Polymer Solutions, *Rheol. Acta* 27 (1988) 656–660.



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